



# Steps for the Optimization of Pipe and Tubing Extrusion Dies

By

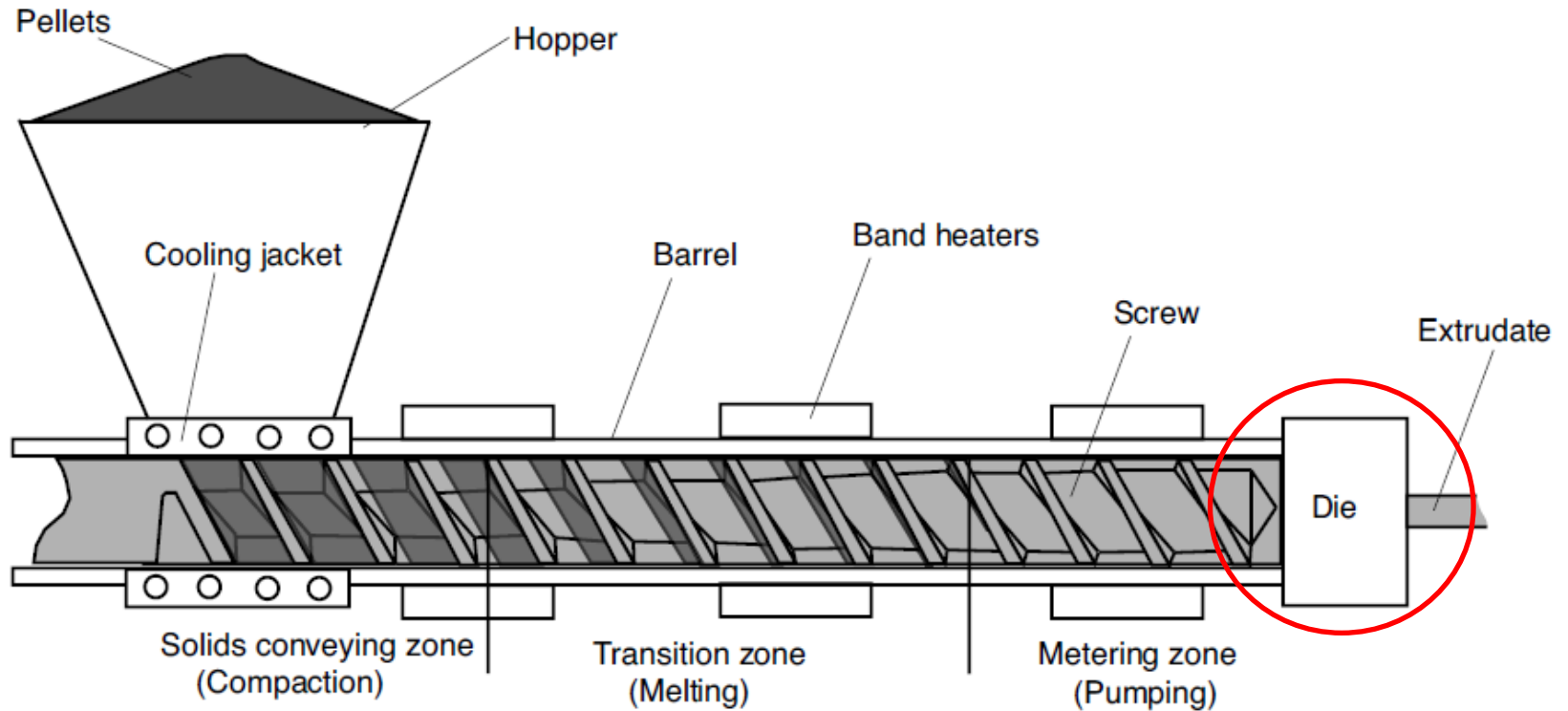
John Puentes  
Tim A. Osswald



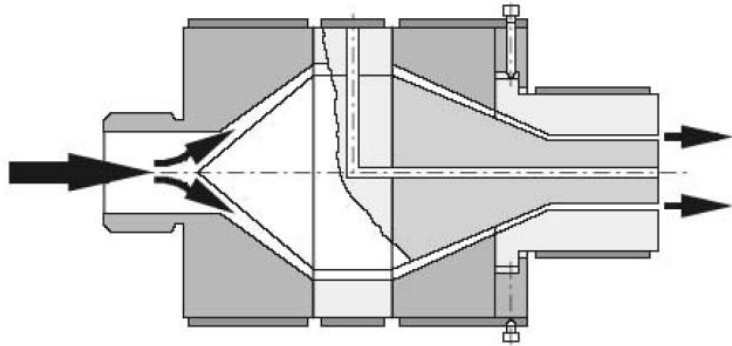
Steve Schick  
Jed Berg



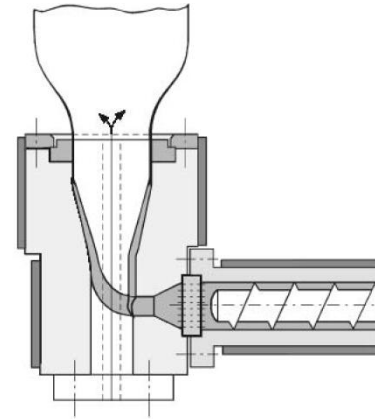
# Extrusion of HDPE pipes



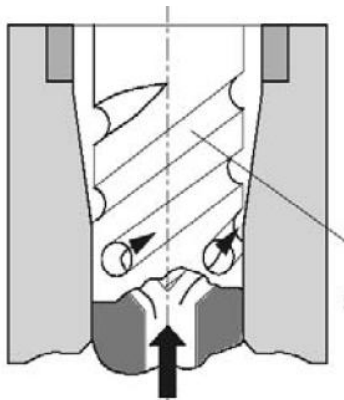
# Pipe and Tubular Dies



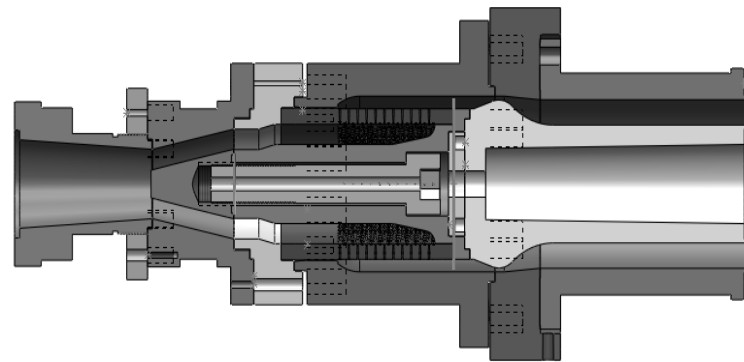
Spider leg tubing die



Cross-head tubing die

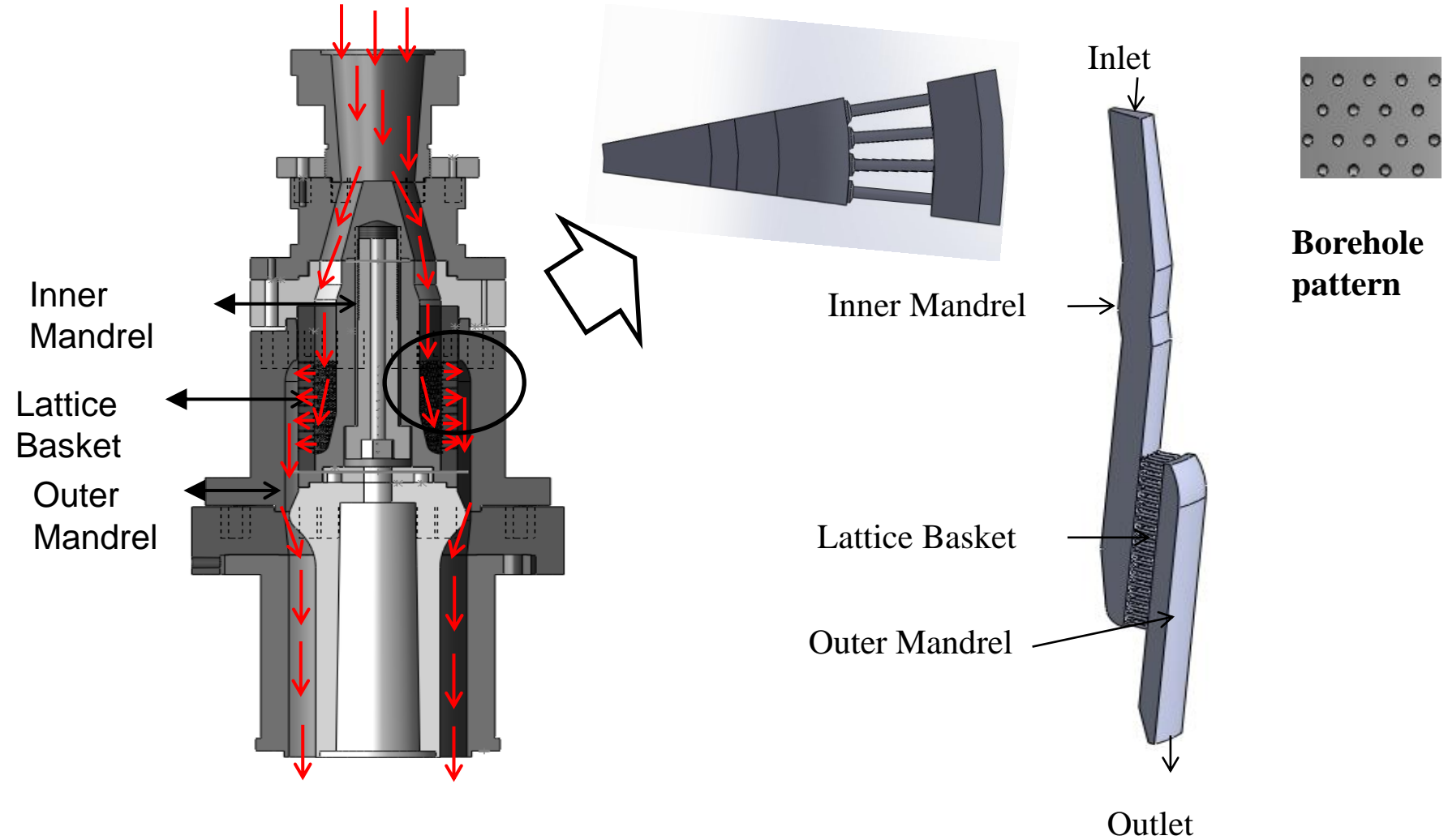


Spiral mandrel



Lattice Basket

# Lattice Basket Die



# Degradation in HDPE

*Chemical reaction*

- \* Temperature history
- \* Shear history
- \* Longer Residence time
- \* Oxygen
- \* Catalyst residuals

*Detection of degradation in HDPE*

Phillips HDPE (Cross-linking)

MW ↑

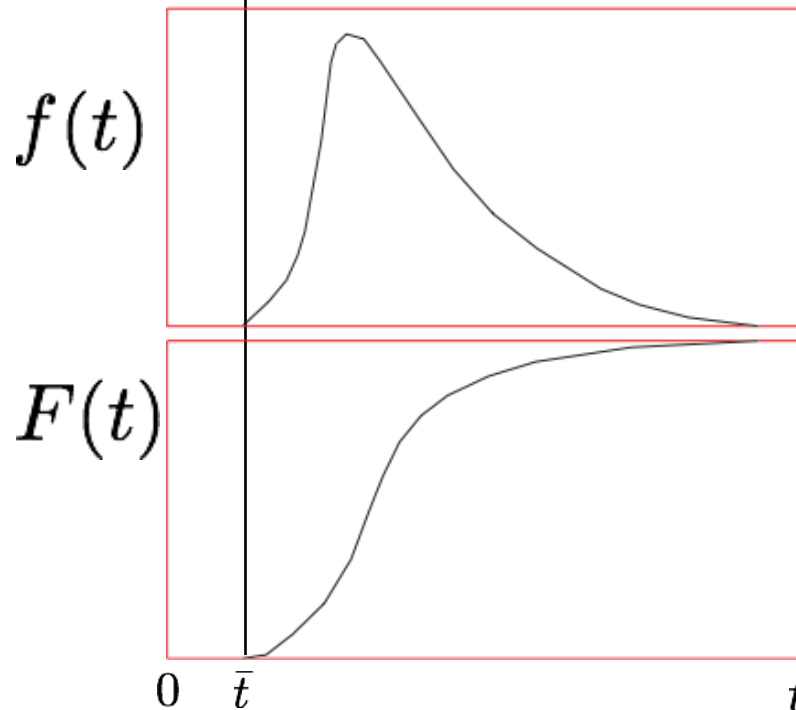
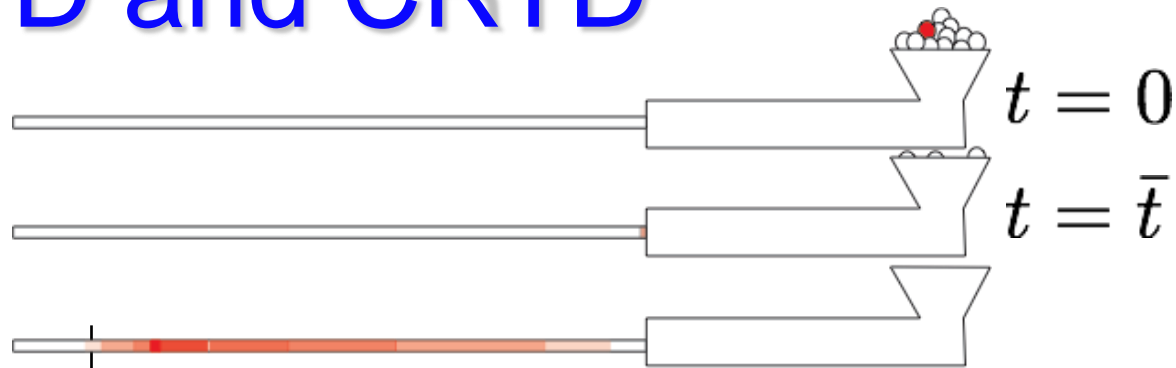
$\eta$  ↑

MFI ↓

Gelation  
(small  
blemishes)



# RTD and CRTD



Residence Time  
Distribution (RTD)

Cumulative Residence  
Time Distribution (CRTD)

$$F(t) = \int_0^t f(t) dt$$

# Processing conditions

**Material:**

*Chevron Phillips Marlex HHM 5202 HDPE*

Property	Symbol	English	S	SI	
<i>Mass Flow Rate:</i>	$\dot{m}$	450	<b>lb./h</b>	0.0567	<b>m/s</b>
<i>Diameter of the extruder:</i>	$D$	3.5	<b>in</b>	0.0889	<b>m</b>
<i>Temperature of the extrudate:</i>	$T$	362	<b>F</b>	183.3	<b>°C</b>
<i>Melt pressure:</i>	$P$	1925	<b>Psi</b>	13.72	<b>Mpa</b>
<i>Time to reach steady state:</i>	$t$	2	<b>h</b>	7200	<b>s</b>

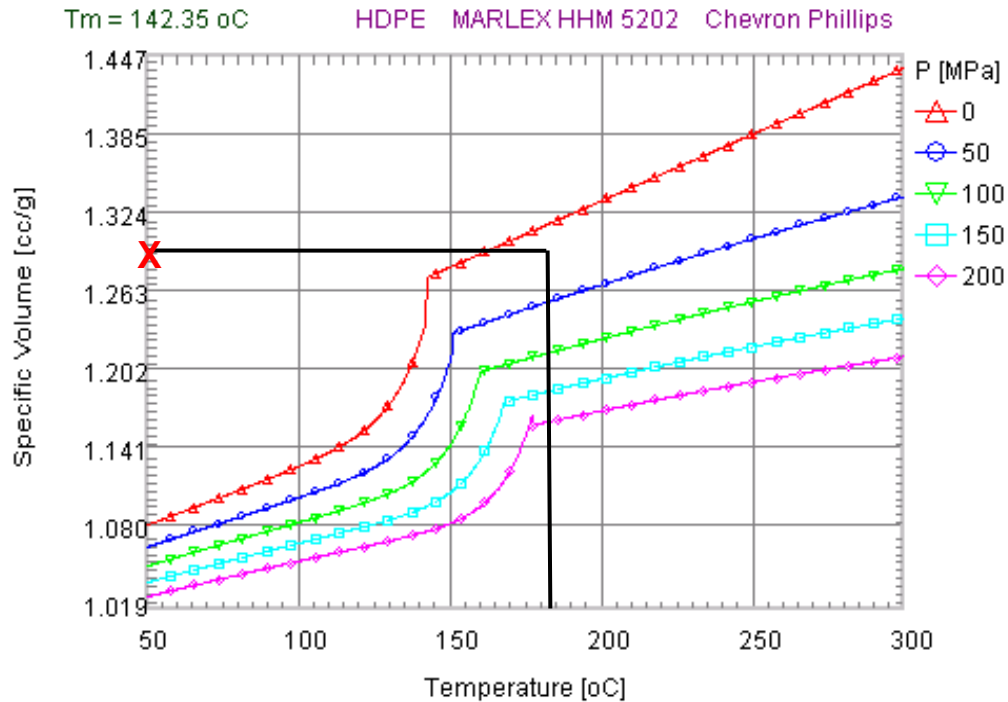
## Carreau Model

<i>Shear rate range</i>	$\dot{\gamma}$	10-14000	$s^{-1}$
<i>power law index</i>	$n$	0.3	<i>dim.</i>
<i>time constant</i>		0.0259	$s$
<i>zero shear rate viscosity</i>	$\eta_0$	5600	$(N * s)/m^2$
<i>infinite shear rate viscosity</i>	$\eta_\infty$	0	$(N * s)/m^2$

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1. Parameters provided by TEEL Plastics, Inc.

# Processing conditions



**Property**

**Symbol**

**English S**

**SI**

Density (T=183.3 °C):  
(By using the PVT diagram)

$\rho$

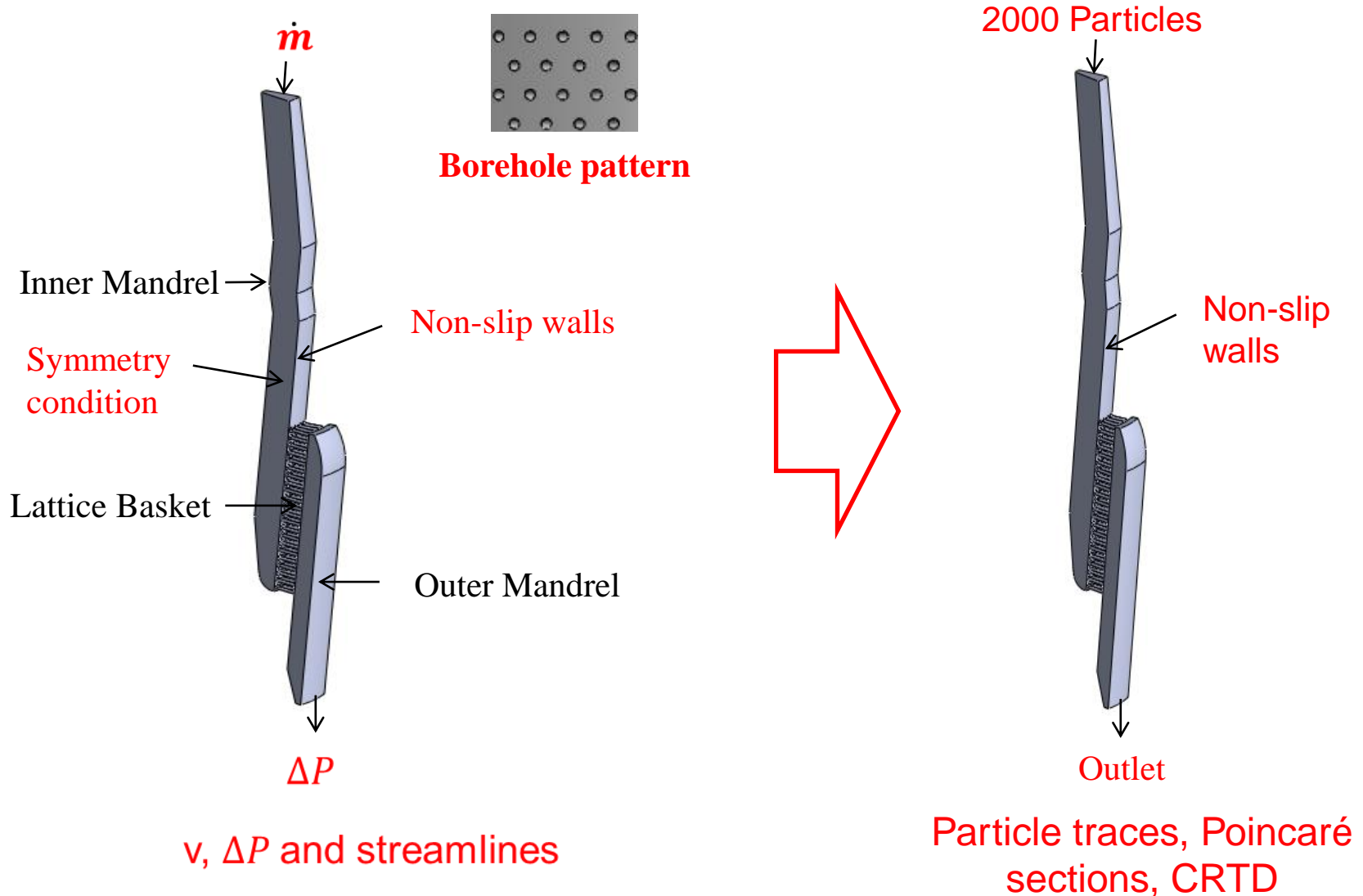
47.837518 lb./ft<sup>3</sup>

766.2835 kg/m<sup>3</sup>

2 Data obtained from Database MOLDEX 3D Molding Innovation



# Lattice Basket simulation



# Mathematical model

## Assumptions

3D model

$$\nabla \cdot \mathbf{u} = 0 \quad (1)$$

Steady state

$$0 = -\nabla p - [\nabla \cdot \boldsymbol{\tau}] \quad (2)$$

Inertia F. - negligible  $Re \ll 1$

Body Forces - negligible  $Ps \ll 1$

$$\boldsymbol{\tau} = \eta \dot{\boldsymbol{\gamma}} \quad (3)$$

Isothermal stage

$$\dot{\boldsymbol{\gamma}} = \frac{1}{2}(\nabla \mathbf{u} + (\nabla \mathbf{u})^t) \quad (4)$$

Bird-Carreau model

$$\frac{\eta - \eta_0}{\eta - \eta_\infty} = [1 + (\lambda \cdot \dot{\boldsymbol{\gamma}})^2]^{\frac{(n-1)}{2}} \quad (5)$$

## Boundary Conditions

*Inlet:* Constant mass flow rate

*Outlet:* Pressure gradient equal to zero

*Walls:* Non-slip

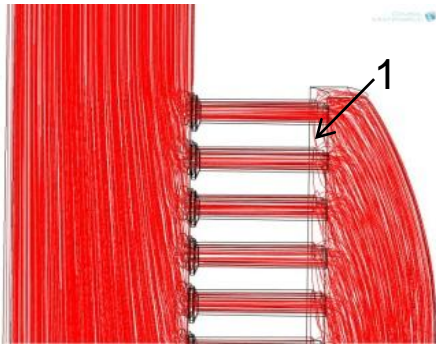
*Cut sides:* symmetry condition

$$\dot{\boldsymbol{\gamma}} = \sqrt{\frac{1}{2}(\dot{\boldsymbol{\gamma}} : \dot{\boldsymbol{\gamma}})} \quad (6)$$

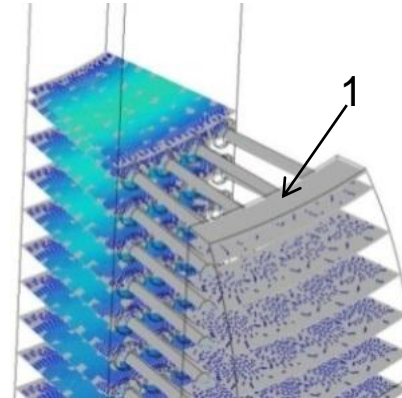


# Implication of the lattice basket

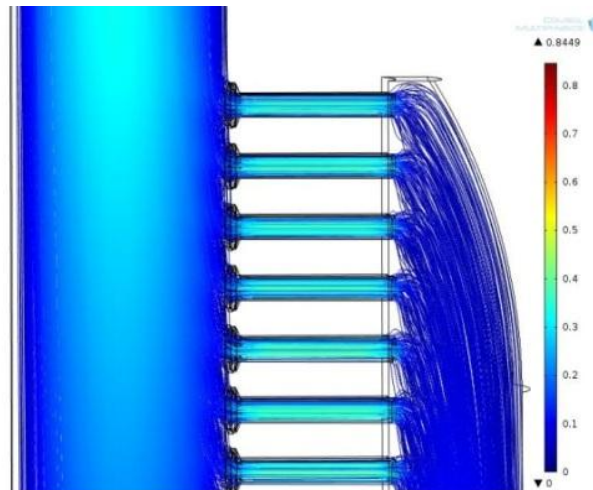
**Streamlines**



**Poincaré sections**

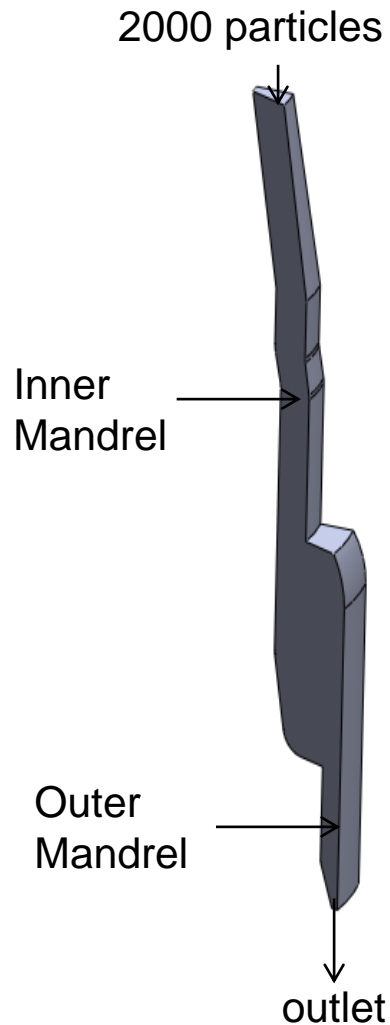


**Tracer curves**

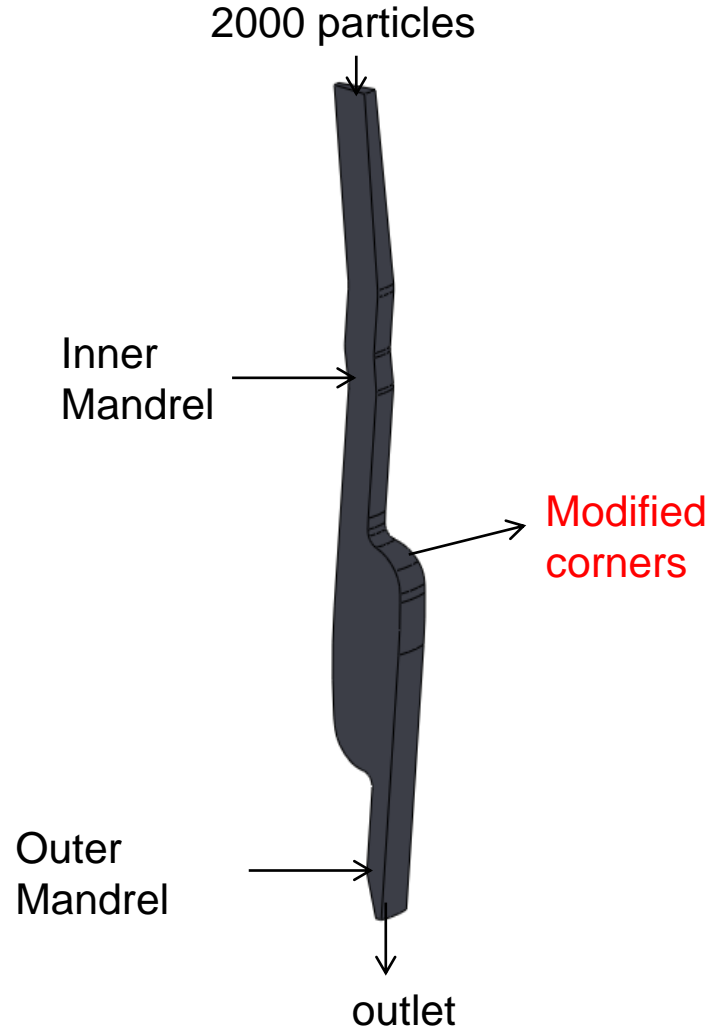


# Baseline for the RTD

Die without lattice



Hypothetical model

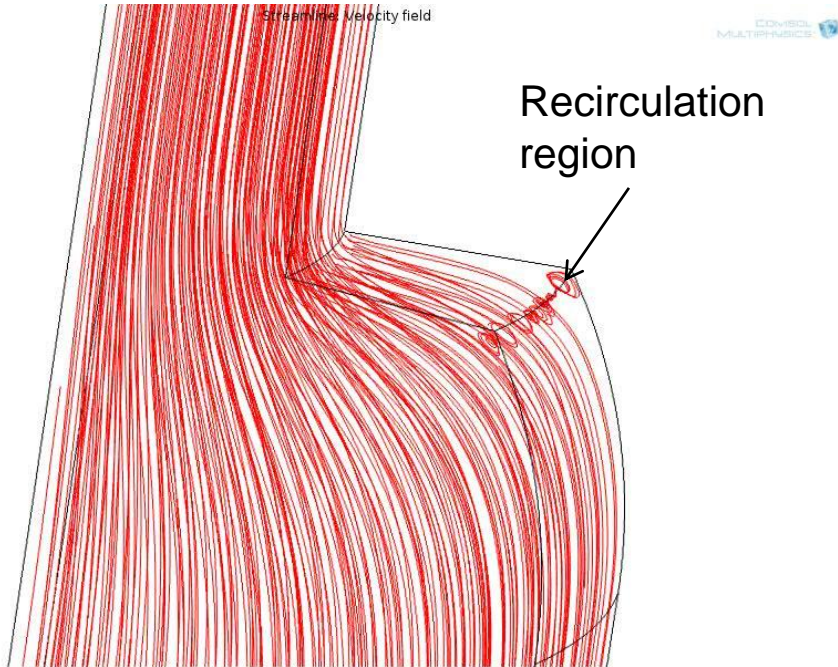




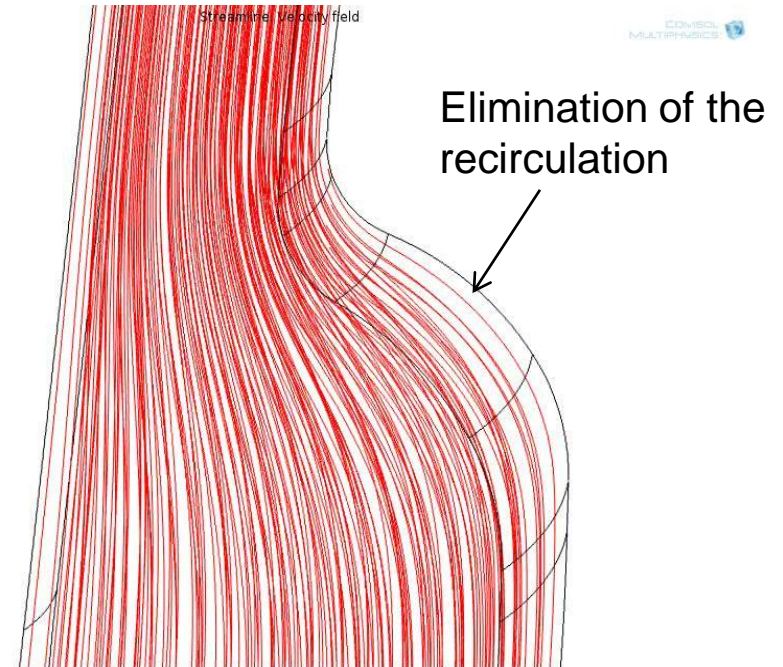
# Implication of the mandrels

## Streamlines

### Die without lattice



### Hypothetical model

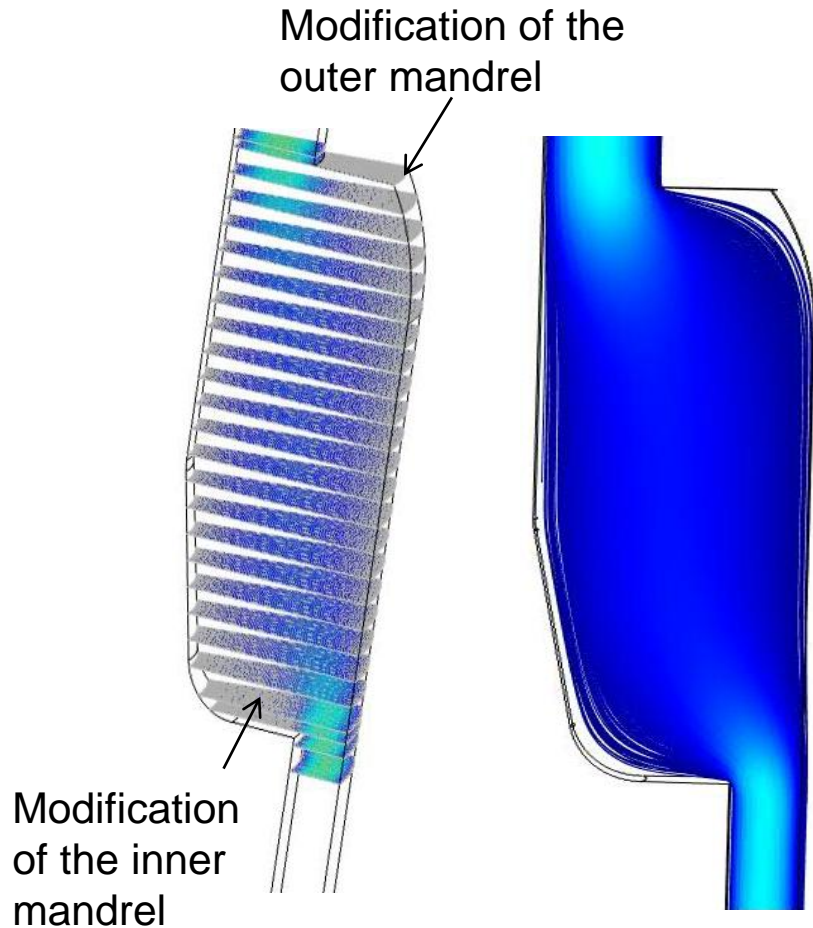




# Implication of the mandrels

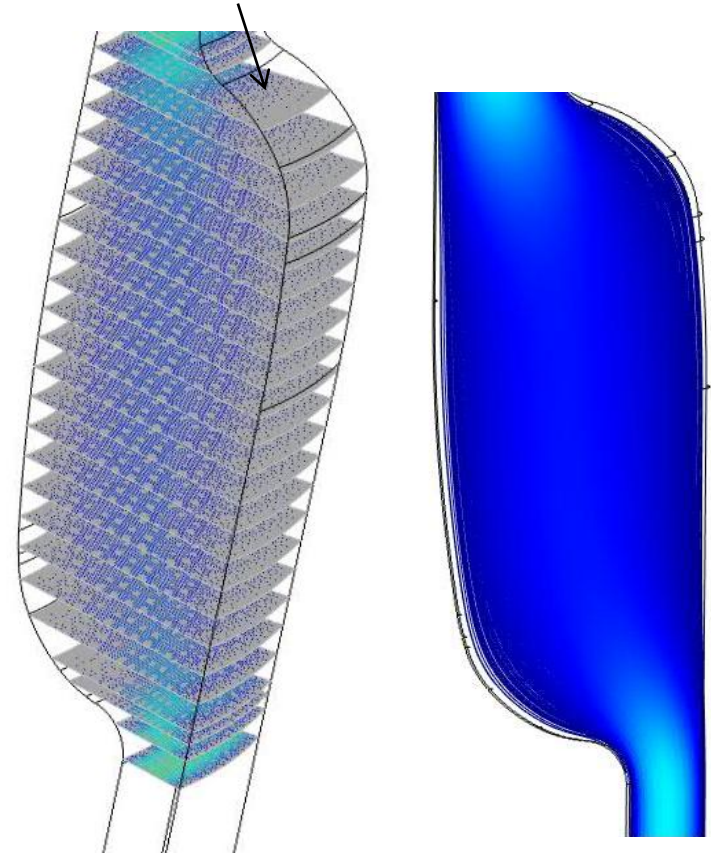
## Particle tracing

### Die without lattice



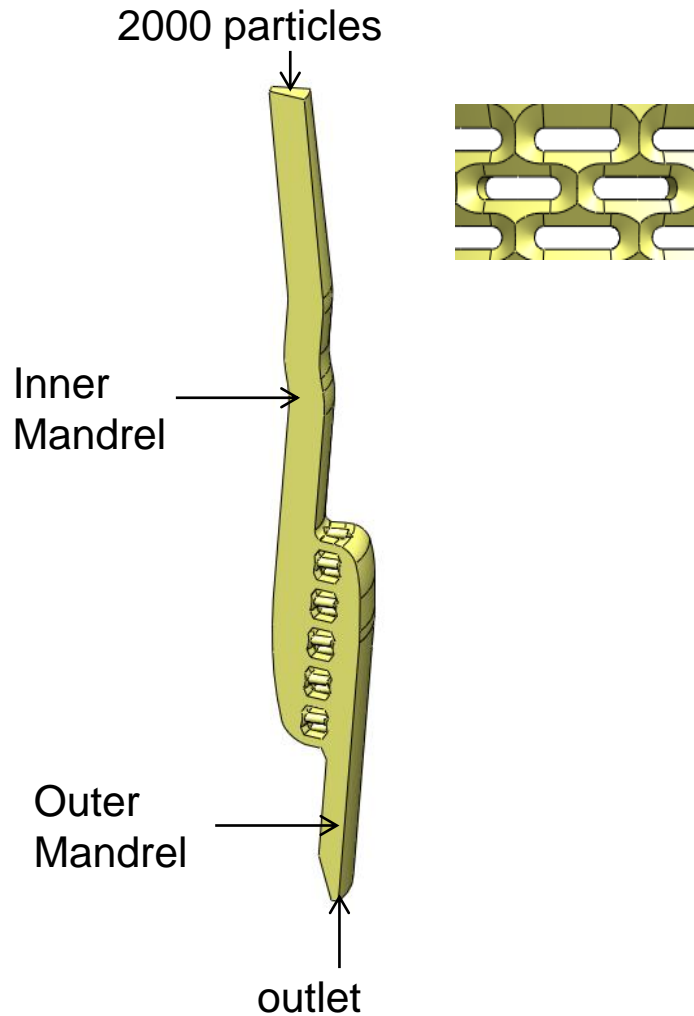
### Hypothetical model

Elimination of zero velocity zones

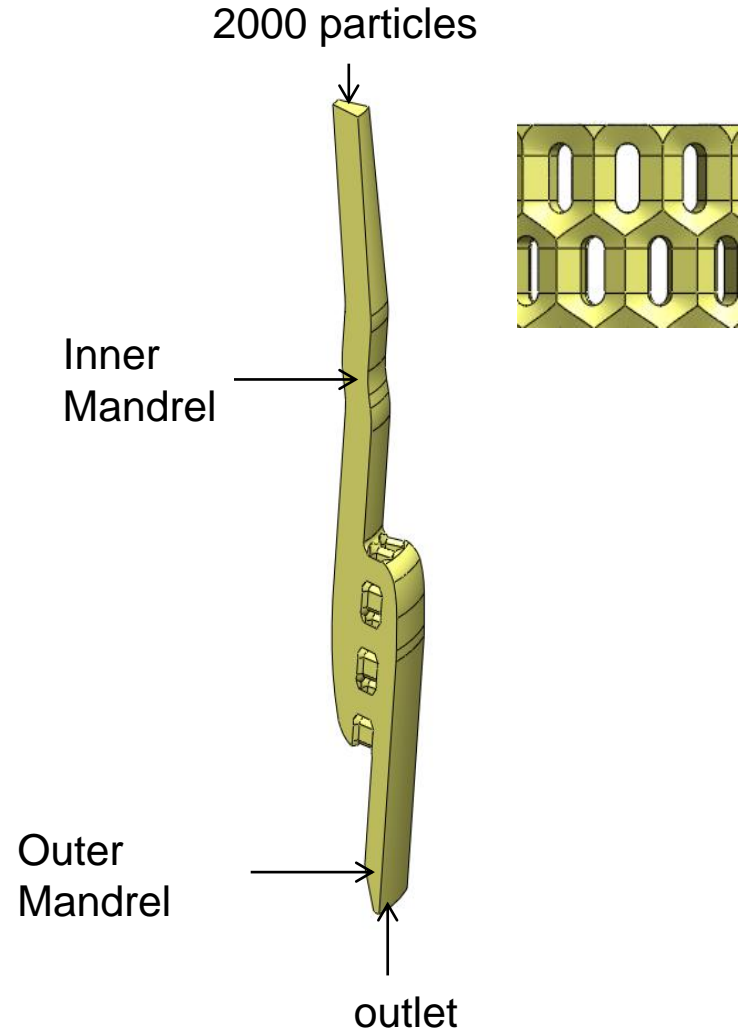


# Optimization of the die

## Slots in a horizontal fashion



## Slots in a vertical fashion

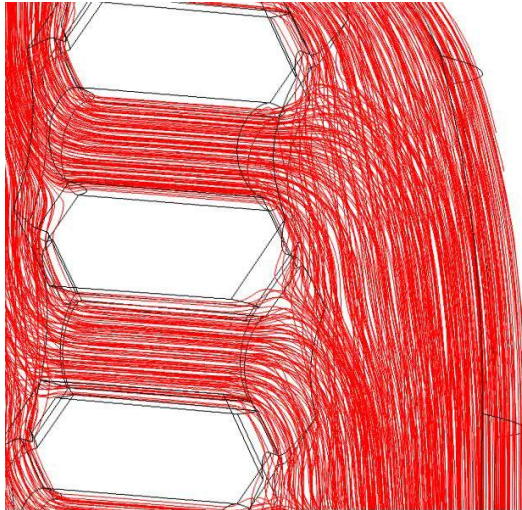




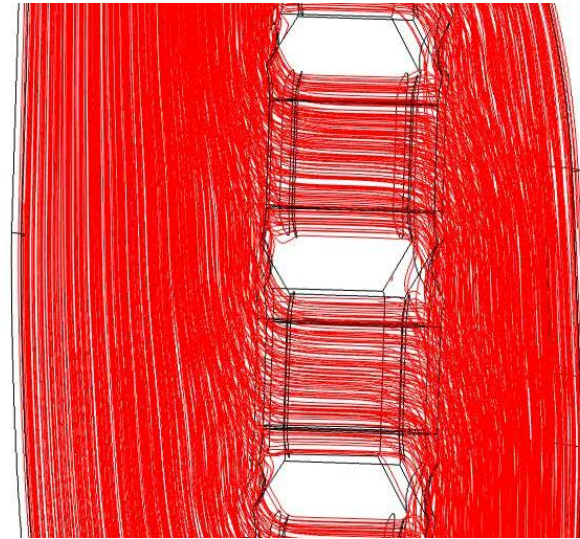
# Novel flow channel profiles

## Streamlines

### Horizontal slots



### Vertical slots



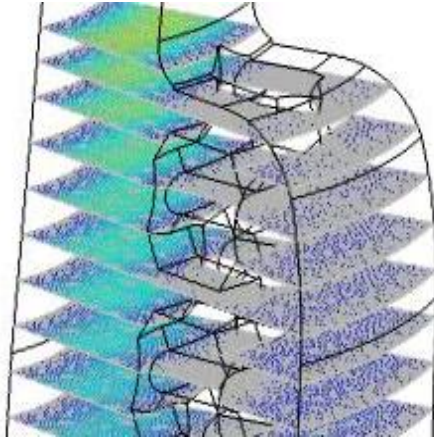




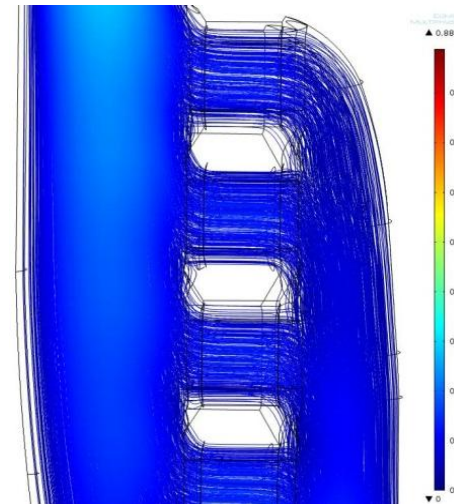
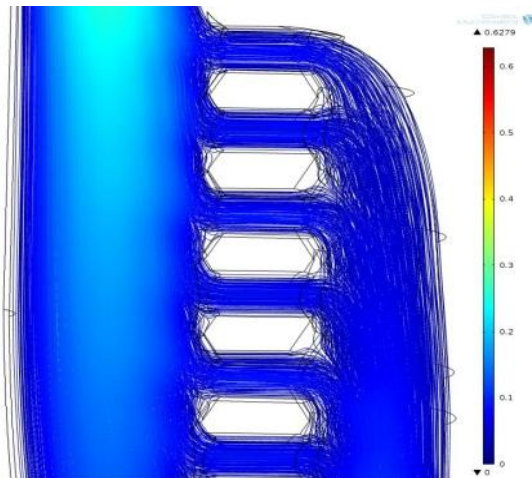
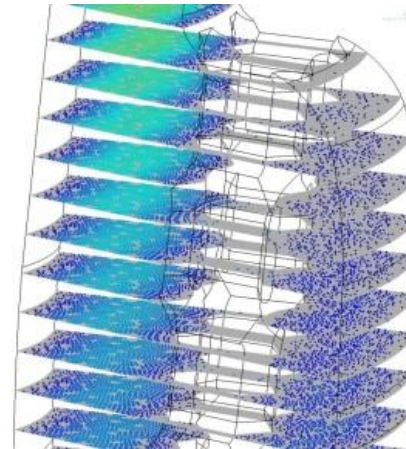
# Novel flow channel profiles

Particle tracking

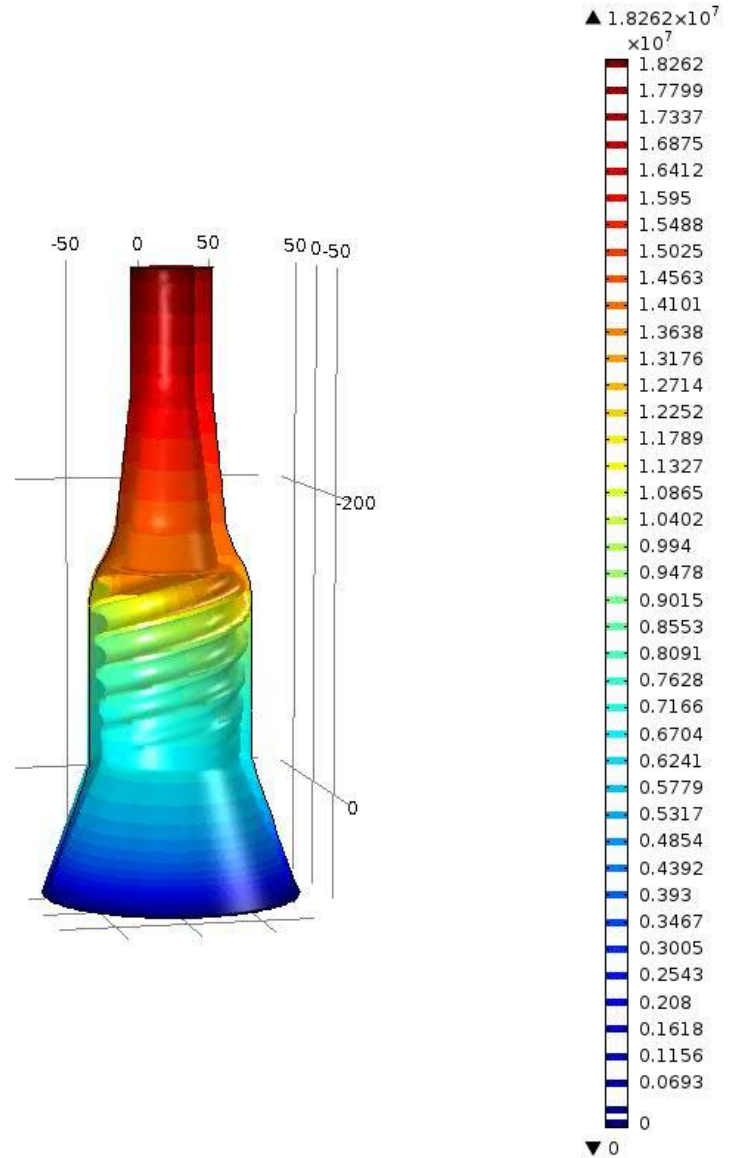
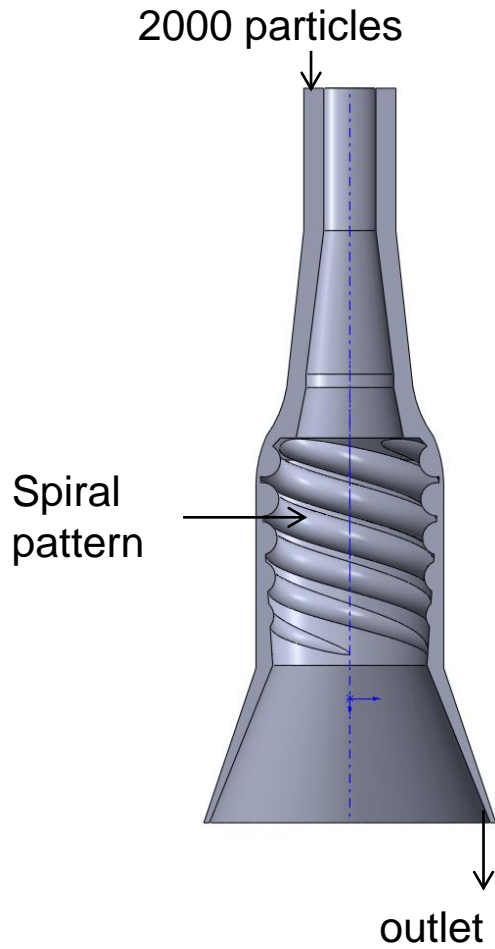
Horizontal pattern



Vertical pattern



# Spiral Mandrel

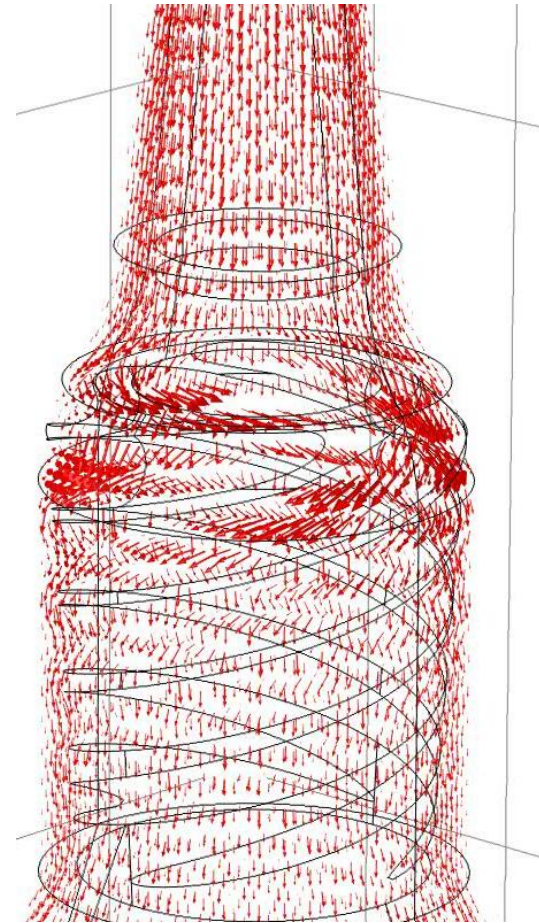
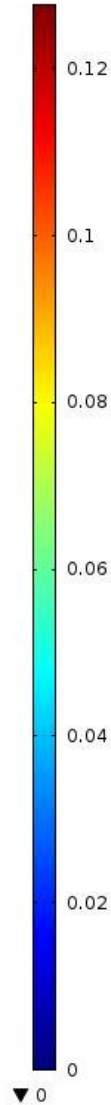
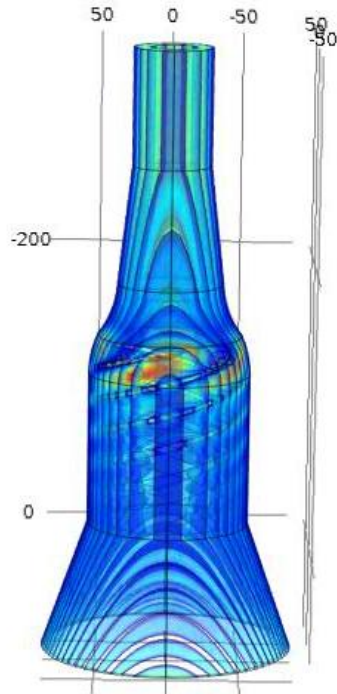




# Spiral Mandrel

▲ 0.1275

## Particle tracing





# CRTD

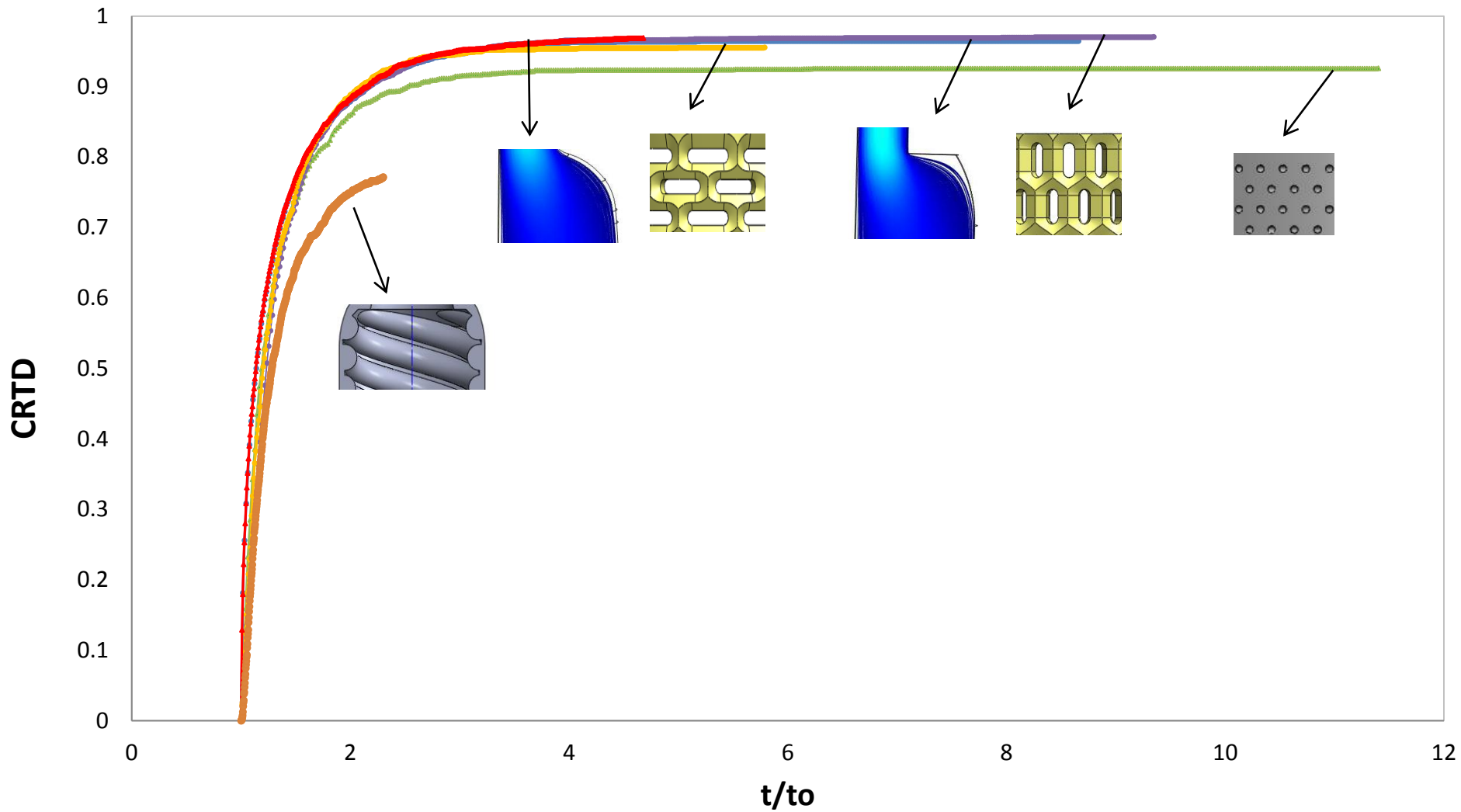
$$\text{Transmission Probability} = \frac{\text{number of particles which reach the outlet}}{\text{number of particles released}}$$

<i>Model</i>	<i>Number of particles released</i>	<i>Particles that reached the outlet</i>	<i>Transmission Probability</i>	<i>Retained particles</i>
<i>Lattice basket die</i>	2000	1852	0.91	148
<i>Die without lattice basket</i>	2000	1929	0.9645	71
<i>Hypothetical model</i>	2000	1939	0.9695	61
<i>Slots in a horizontal fashion</i>	2000	1911	0.9555	89
<i>Slots in a vertical fashion</i>	2000	1941	0.9705	59
<i>Spiral Mandrel</i>	2000	1543	0.7715	457





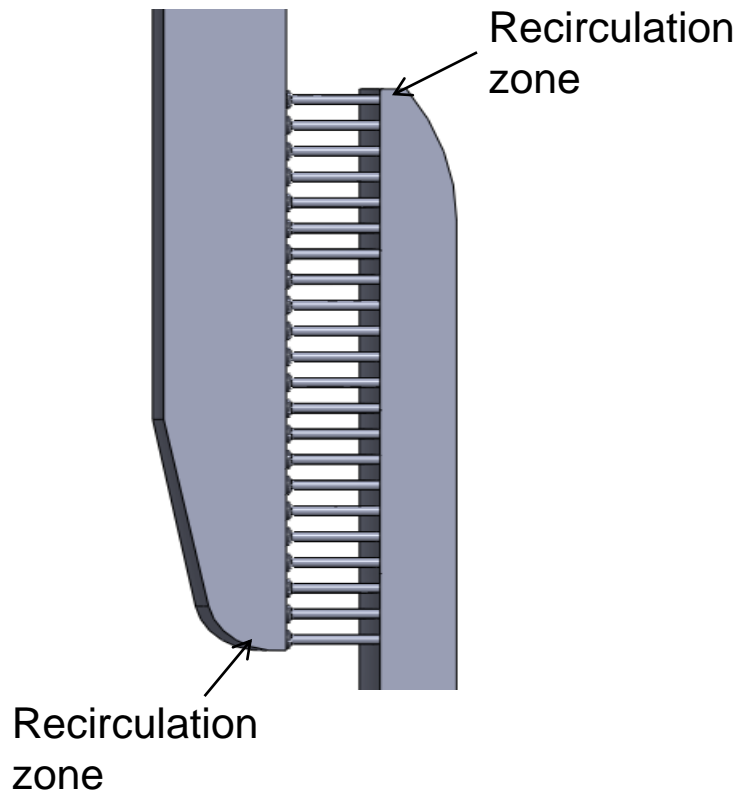
# CRTD



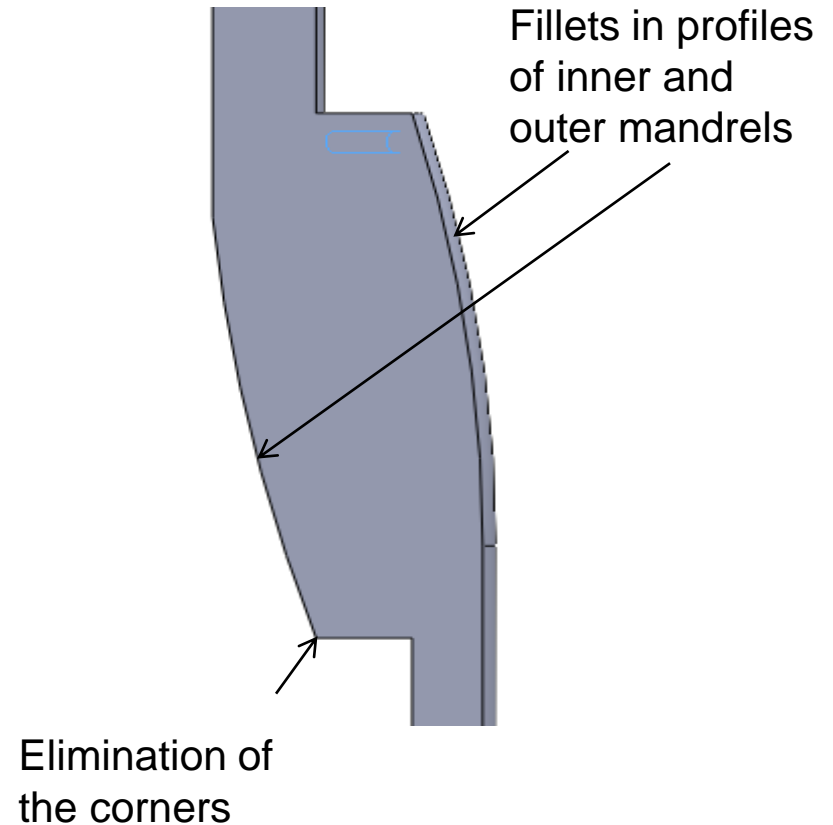


# Mechanical Design improvements

## Previous mandrel design



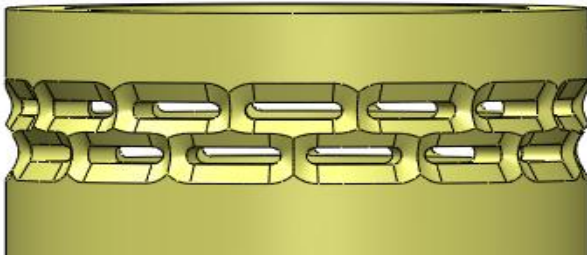
## Possible solution



# Mechanical Design improvements



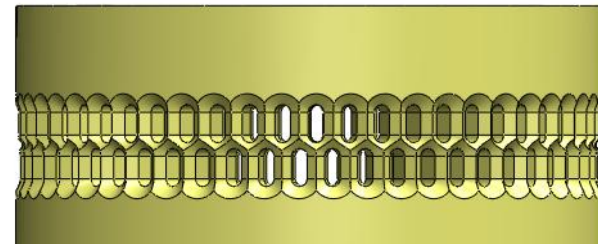
Lattice basket



Horizontal Slots

↓ RTD 50%

60% less retention of material



Vertical Slots

↓ RTD 75%

3 times less retention of material

Smaller pressure losses

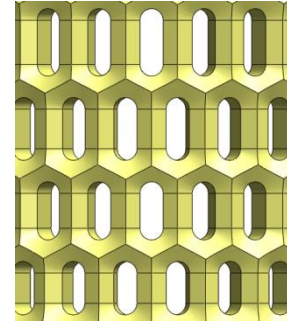
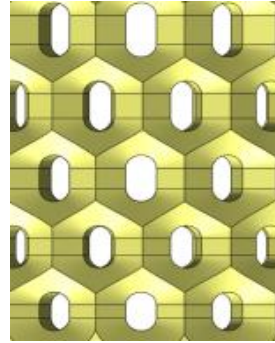
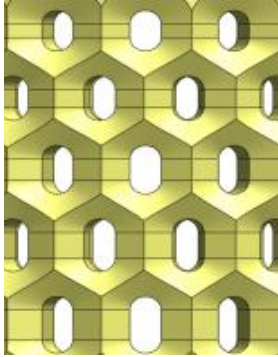
Lower Power requirements for the same operation conditions

Higher volumetric flow rates

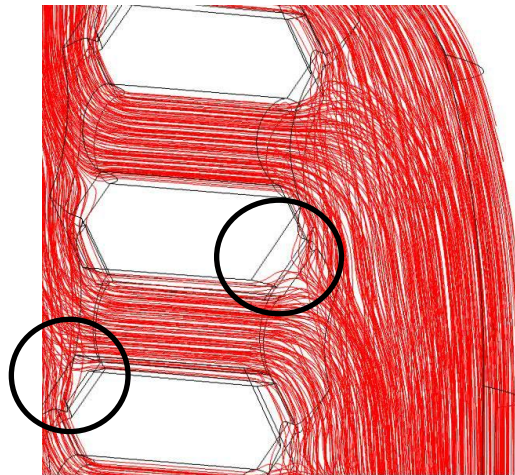


# Future Work

## Velocity profile



## Structural analysis



COMSOL  
MULTIPHYSICS





# Future Work

## Isothermal assumption

Analysis of the Brinkman number  $Br = \frac{u^2 \eta}{k \Delta T}$

## Experimentation

Influence of the number of cavities and the area of the cavities in the surface finish and mechanical strength.

<b>Geometry</b>	<b>Number of cavities</b>	<b>Total area (mm<sup>2</sup>)</b>	<b>Ratio of cavities</b>	<b>Ratio of areas</b>
<b><i>Lattice basket</i></b>	2100.00	3.00	1.00	1.00
<b><i>Vertical slots</i></b>	550.00	59.63	3.82	19.85
<b><i>Horizontal slots</i></b>	126.00	108.63	16.67	36.16
<b><i>Spiral mandrel</i></b>	4.00	127.68	525.00	42.50





The authors are grateful to TEEL Plastics Inc. for the technological and financial support in this project.



Thanks to all the members of the PEC



Thanks to technical support of COMSOL Multiphysics.





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Database MOLDEX 3D

<http://www.matweb.com/search/datasheetText.aspx?bassnum=PEHM29>

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