

# Chrome Plating Process Optimization

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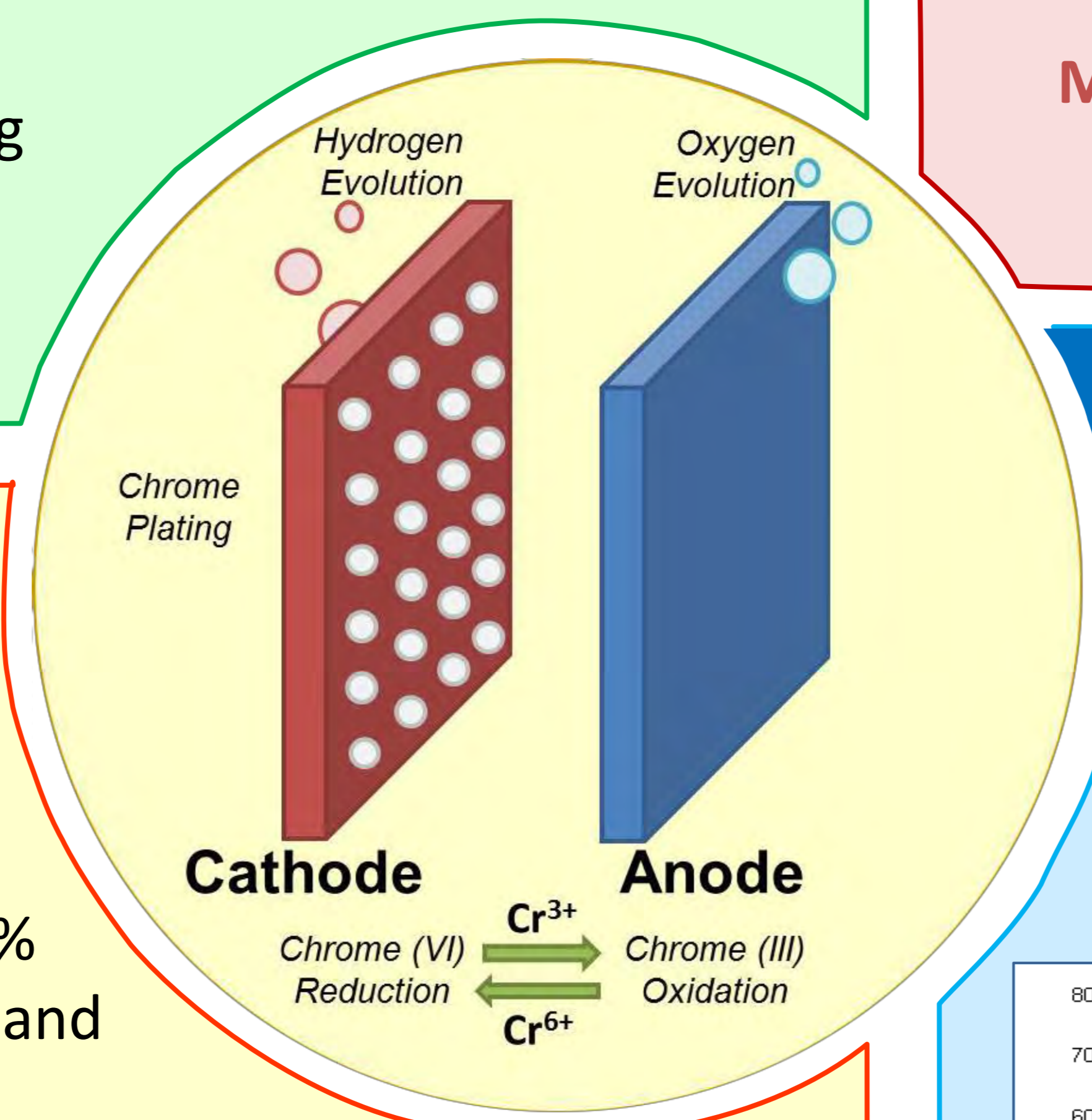
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## Problem Definition

**Motivation:** Lack of a computer model leads to poor understanding of the process, resulting in energy and material waste

**Objective:** Model an existing chrome plating process in COMSOL to meet client specifications

**Goal:** Use model to optimize operating conditions and realize chrome and energy savings



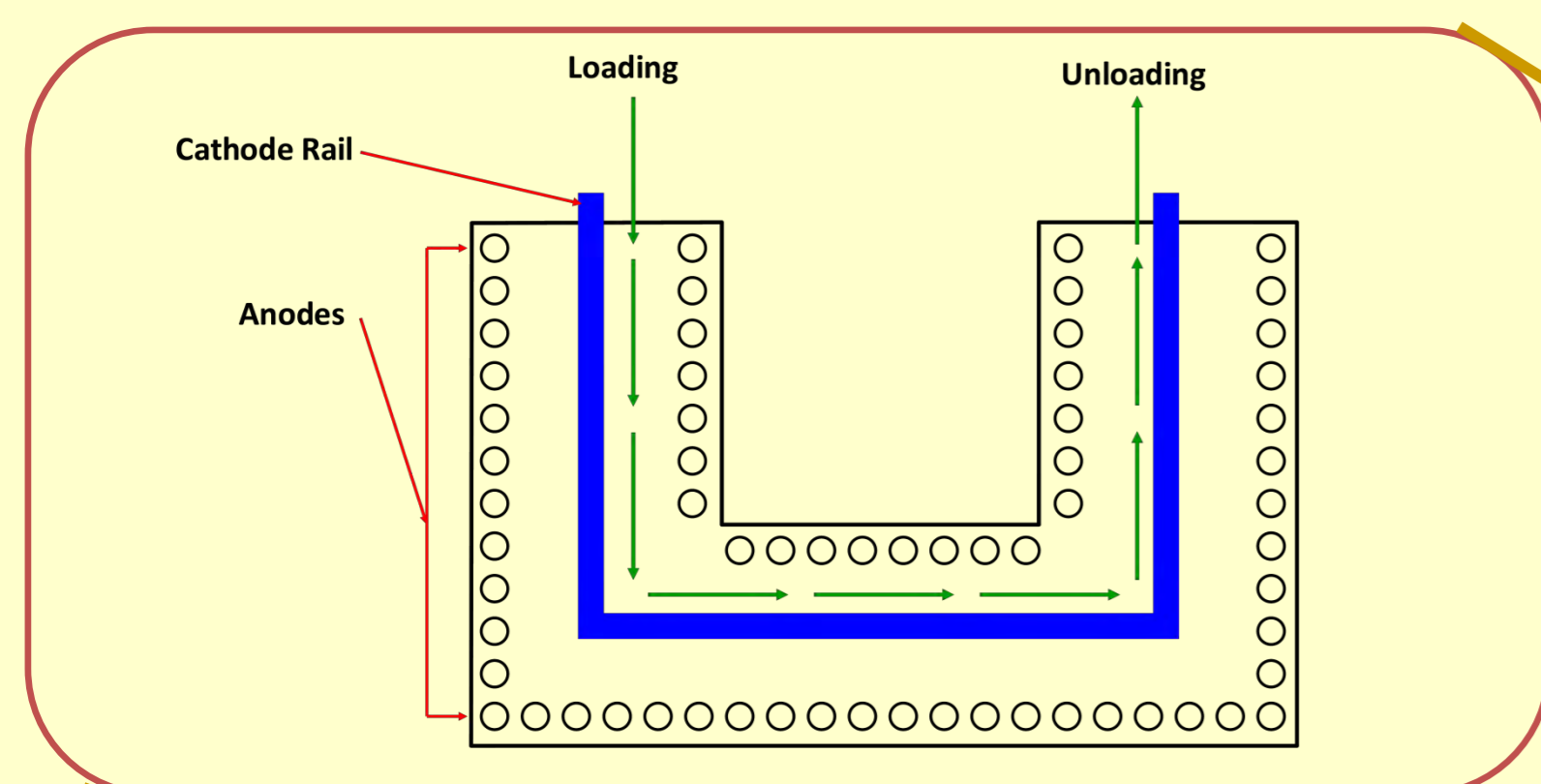
## Background

Plating occurs in two steps:

1. Dichromate reduces to Cr<sup>3+</sup>
2. Cr<sup>3+</sup> reduces to Cr<sup>0</sup>

Current efficiency of plating is only 15% due to competing hydrogen evolution and Cr<sup>3+</sup> reduction [1]

Electrode	Material	Reactions
Cathode	Stainless Steel	$Cr^{3+} + 3e^- \rightarrow Cr^0$ $2H^+ + 2e^- \rightarrow H_2$ $(Cr_2O_7)^{2-} + 6e^- + 14H^+ \rightarrow 2Cr^{3+} + 7H_2O$
Anode	Lead (Inert)	$2H_2O \rightarrow 4H^+ + 4e^- + O_2$ $2Cr^{3+} + 7H_2O \rightarrow (Cr_2O_7)^{2-} + 6e^- + 14H^+$



Rinse	Rinse	Rinse	Rinse	Rinse	Rinse	Rinse	Rinse	Rinse	Plating Bath
8	7	6	5	4	3	2	1		
			Electro-clean	Rinse 1	Rinse 2	Rinse 3		Reverse Etching	

## Impacts

The model could be used to optimize the plating process and reduce chrome and energy consumption with the following outcomes:

### Environment:

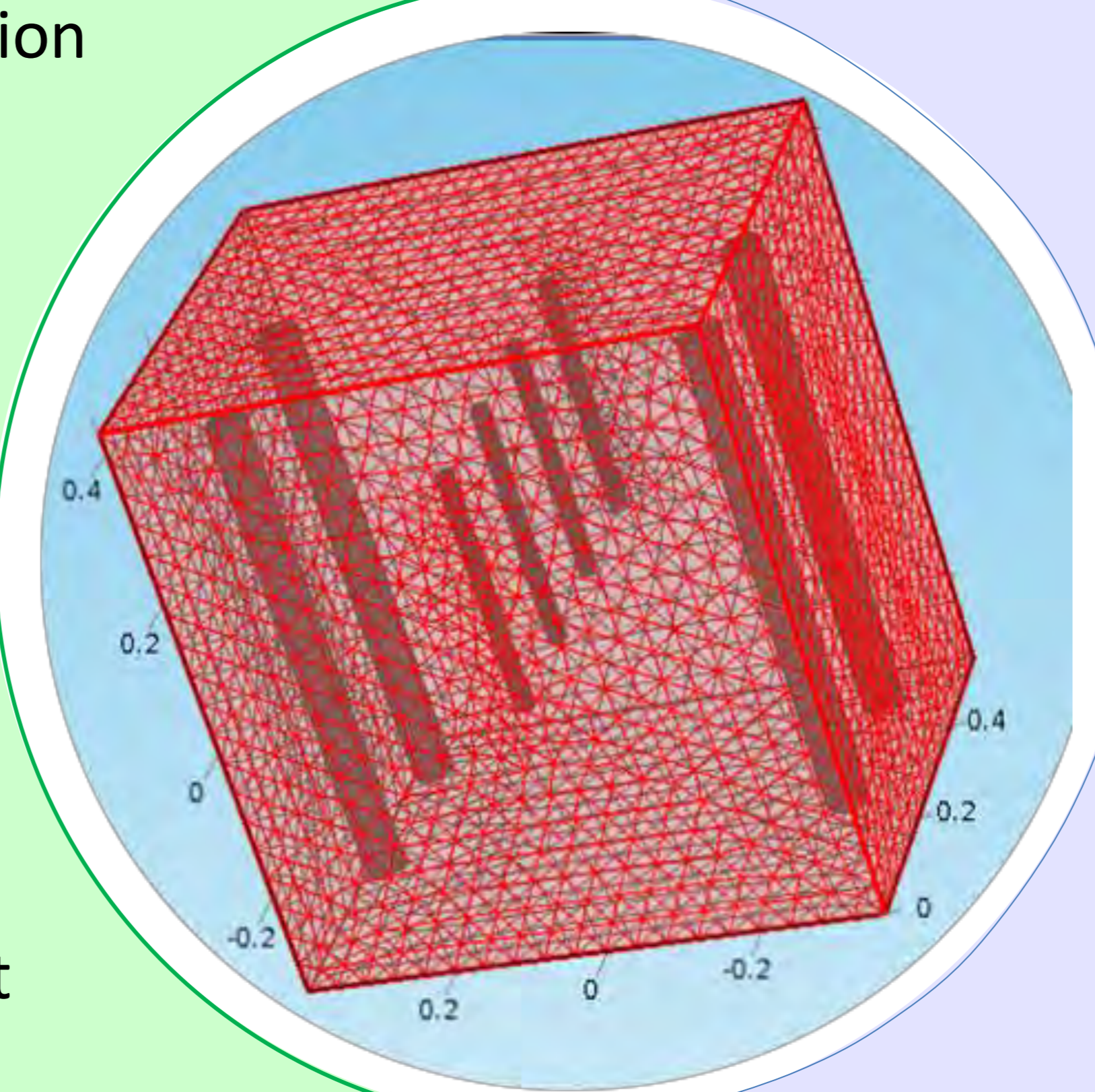
- Reduction of hazardous chrome emissions from the plating bath and the grinding operations
- Reduction of the carbon footprint of the plating process

### Health and Safety:

- Decreased risk of worker exposure to chrome dust

### Economic:

- Cost savings in raw materials (chrome) and utilities



## Model Development

**Model:** Electrodeposition Moving Mesh Module in COMSOL

**Geometry:** 2D, 1 anode, 1 cathode, extremely fine mesh

**Kinetics:** Butler-Volmer at the electrode interface

$$i = i_0 \left[ \exp\left(\frac{\alpha_a n_e F \eta}{RT}\right) - \exp\left(\frac{\alpha_c n_e F \eta}{RT}\right) \right]$$

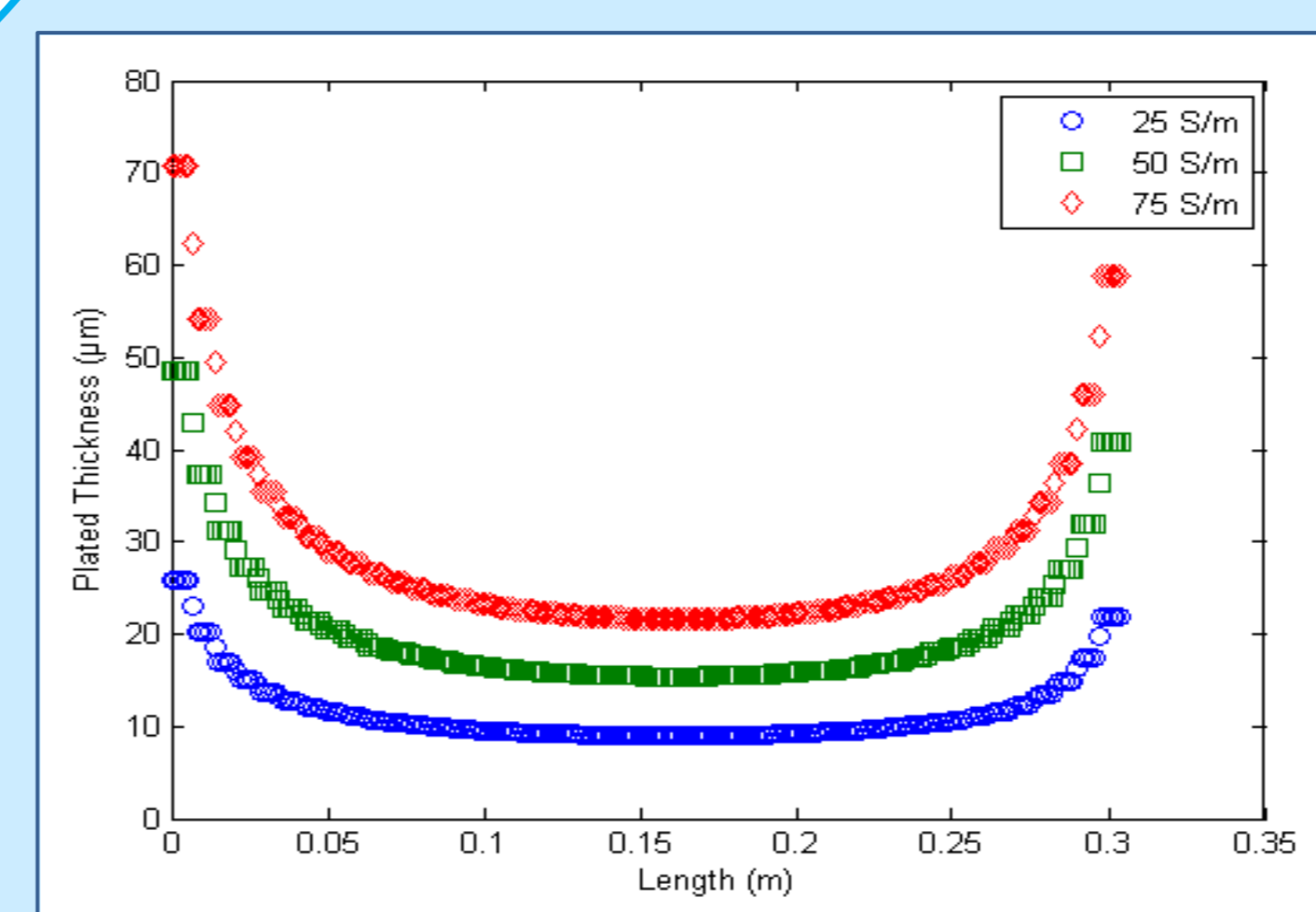
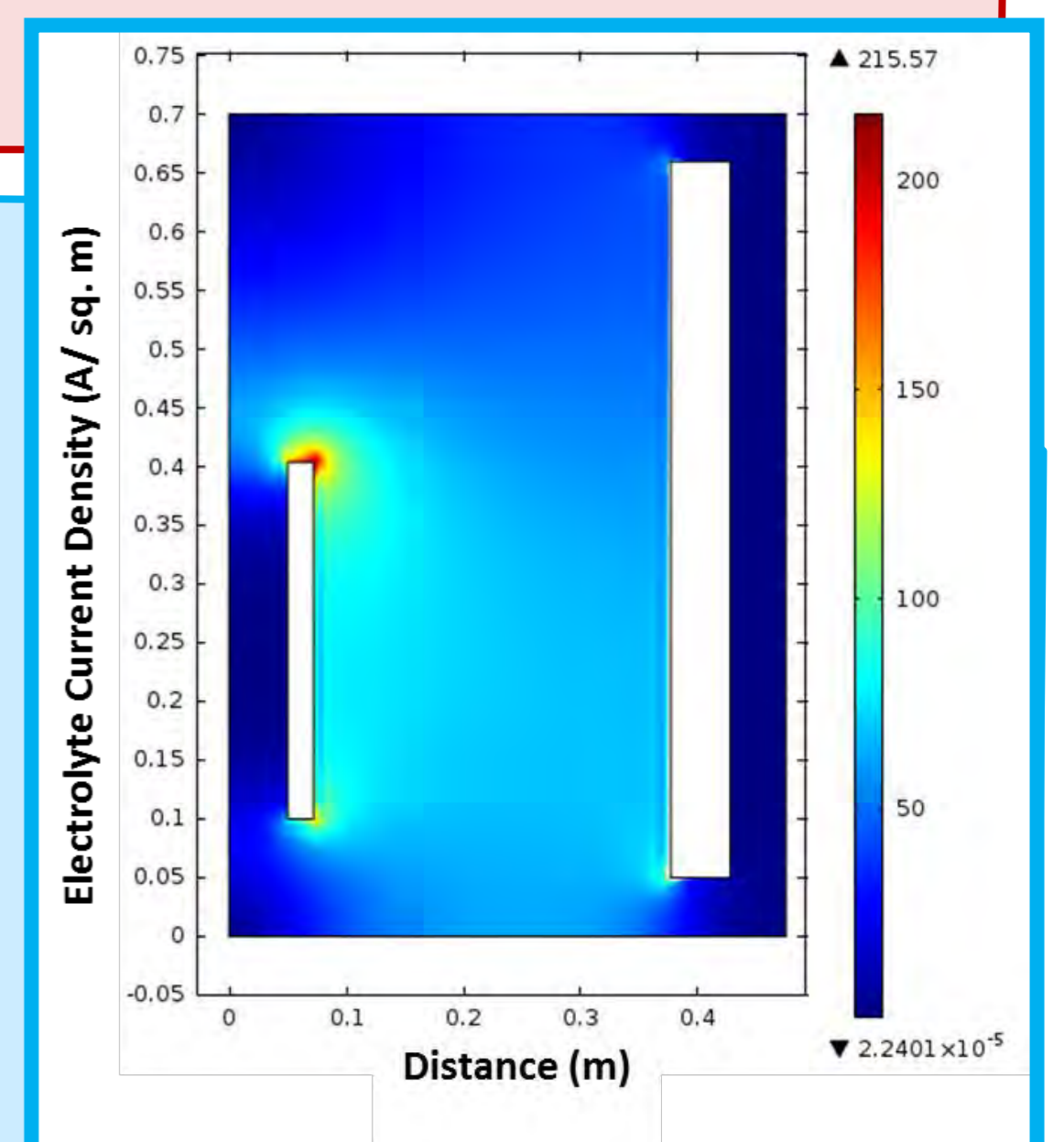
**Mass transfer:** Tertiary Nernst-Planck

$$N_i = -D_i \nabla C_i - z_i u_i F C_i \nabla V$$

Diffusion      Migration

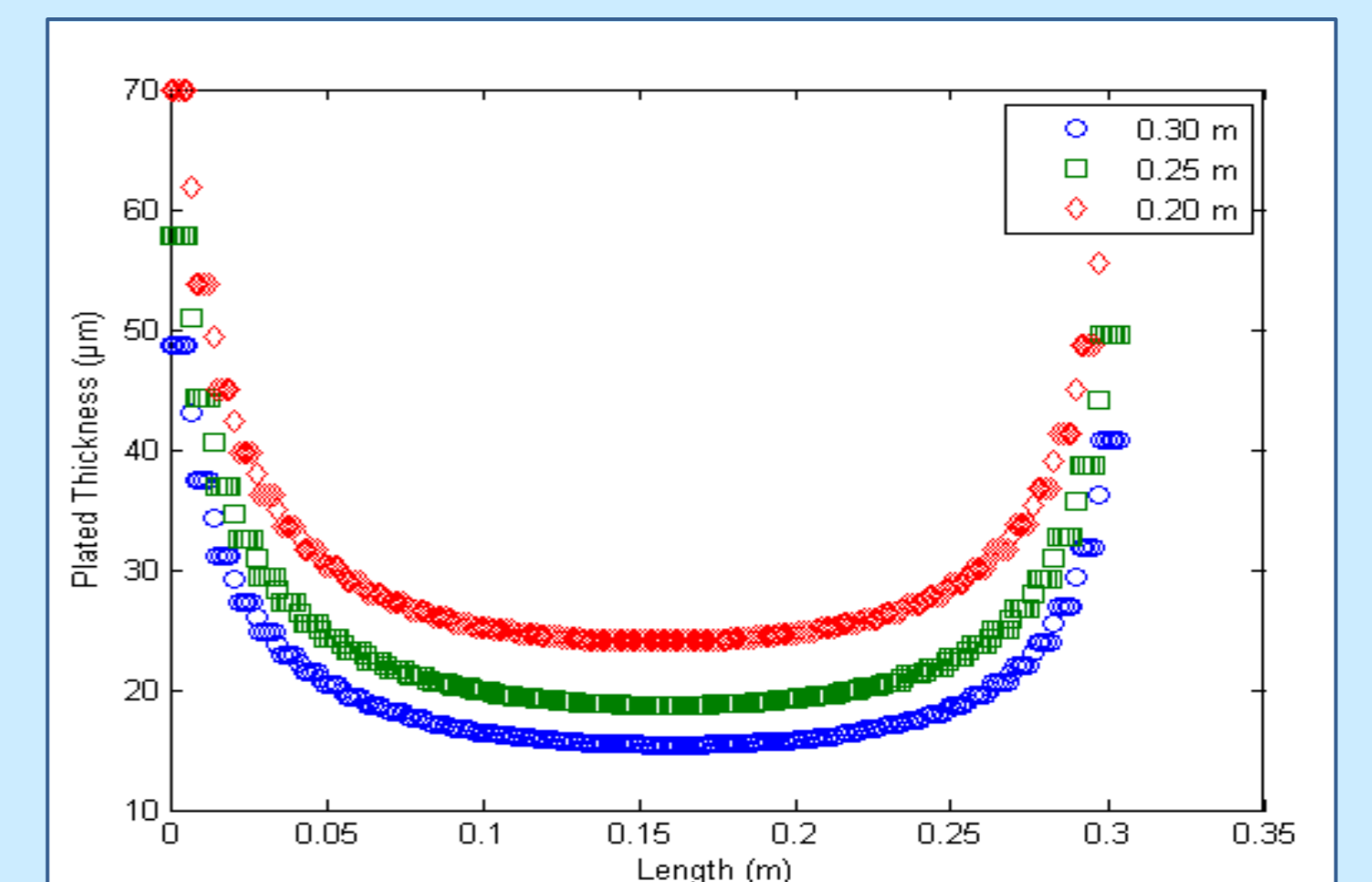
## Results

Current from the excess anode area accumulate at the top and bottom of the cathode

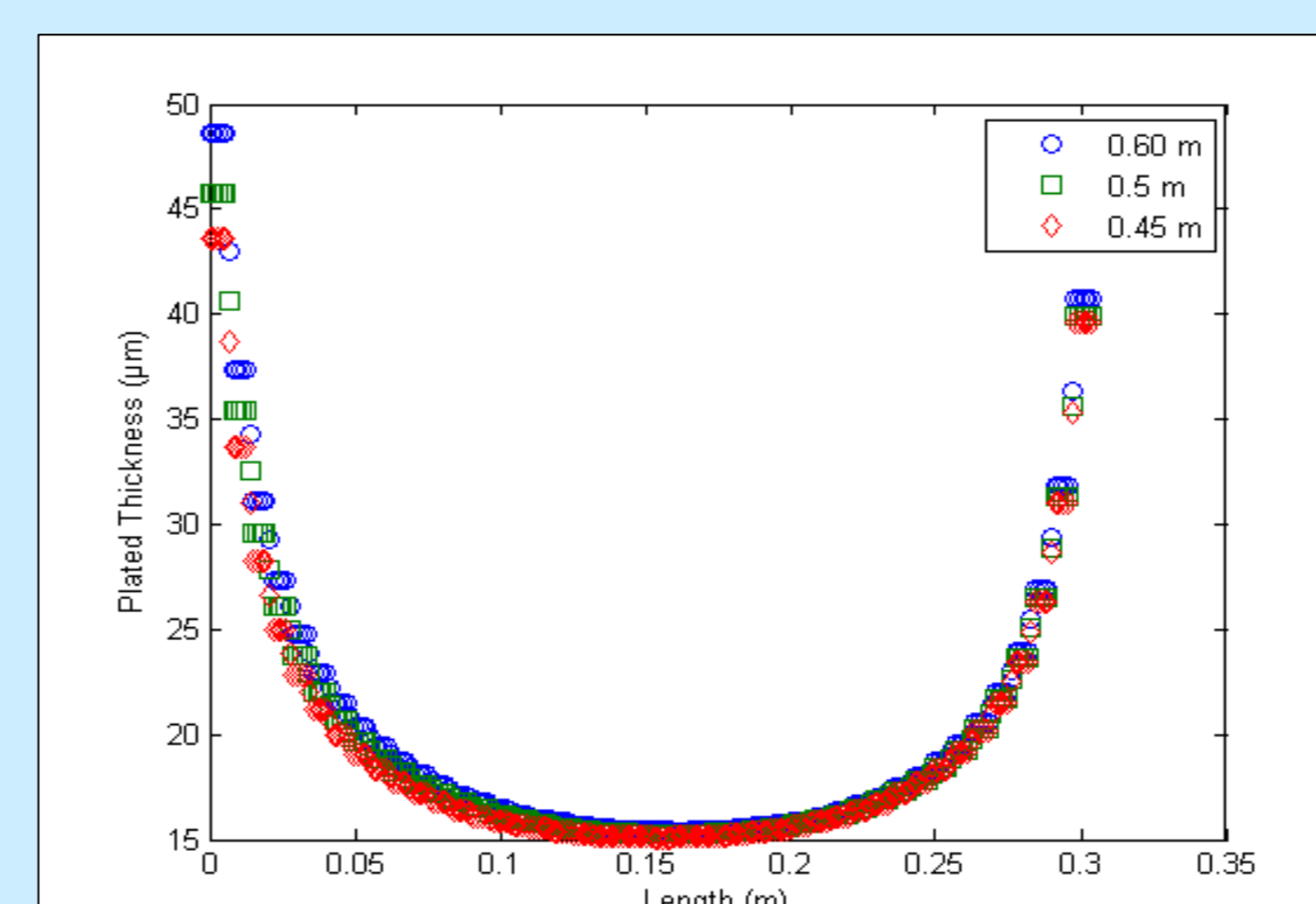


Plating thickness is directly proportional to **solution conductivity** however it also increases non-uniformity at higher values.

An increase in **anode-cathode spacing** decreases the plating thickness. Decreasing this distance results in much less uniformity.



**Anode height** appears to have little effect on plating. Further refinement of the model is required to incorporate process sensitivity to this parameter.



## Next Steps

### Refining the 2D model

- Define system in terms of current density instead of electric potential for higher accuracy
- Include convective forces and effect of gas evolution in mass transfer calculations

### 3D model

- Determine if 3D model is feasible with current computational limitations
- Vary key parameters with a 3D model
- Validation with real process data
- Temperature effects

