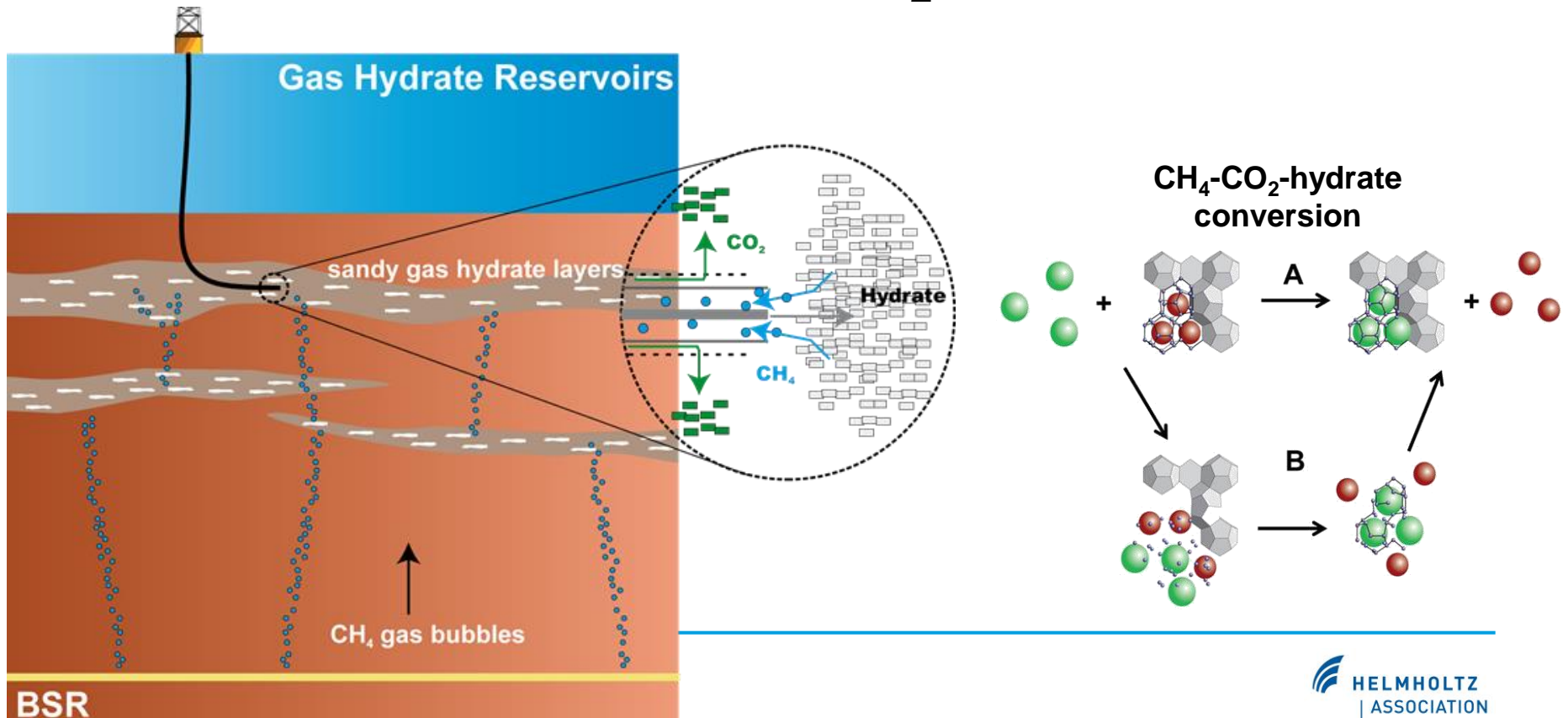
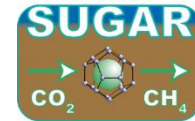




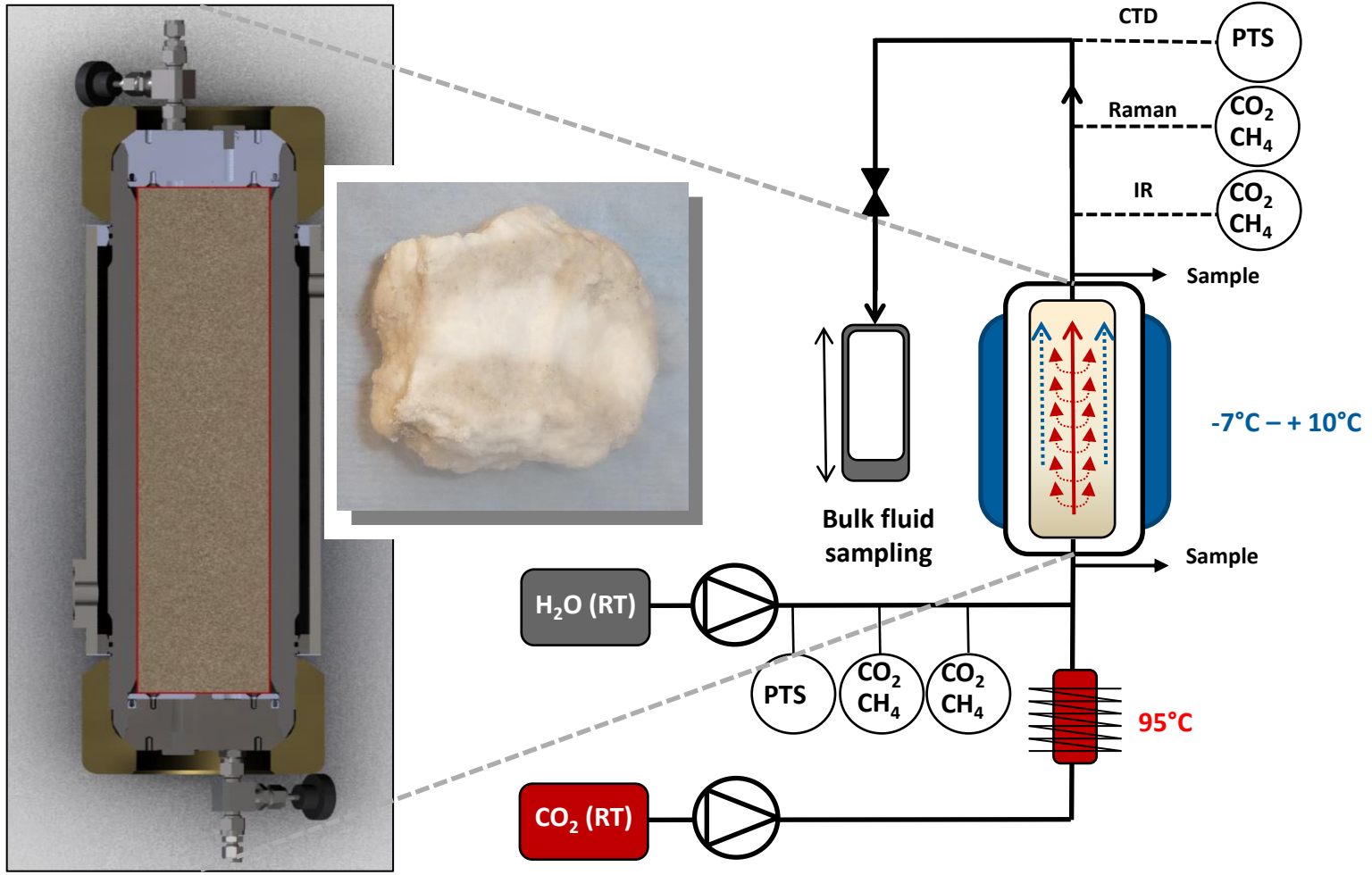
# A COMSOL Multiphysics®-based Model for Simulation of Methane-Hydrate Dissociation by Injection of Superheated CO<sub>2</sub>



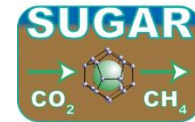
# Experimental setup



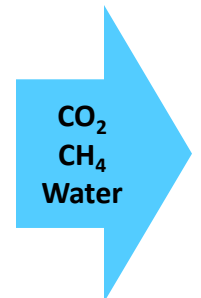
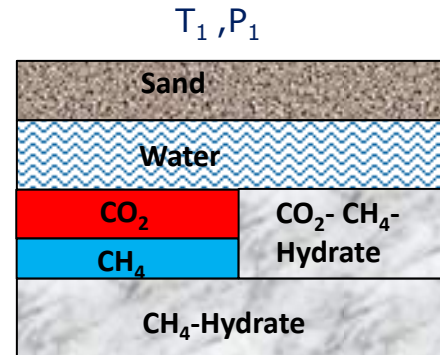
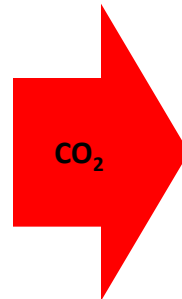
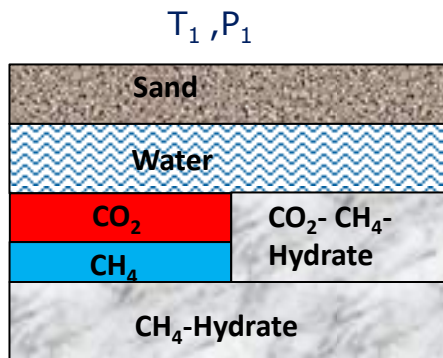
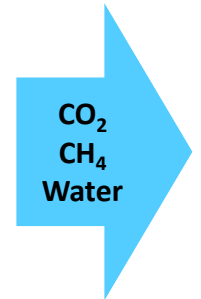
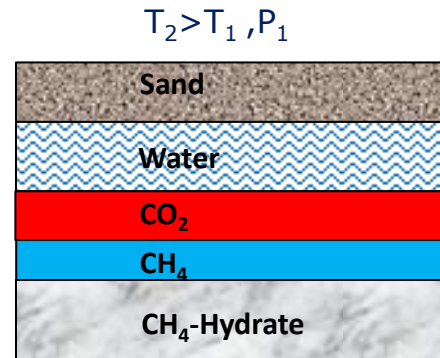
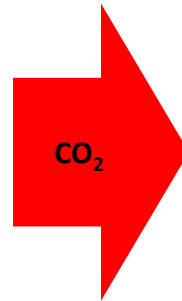
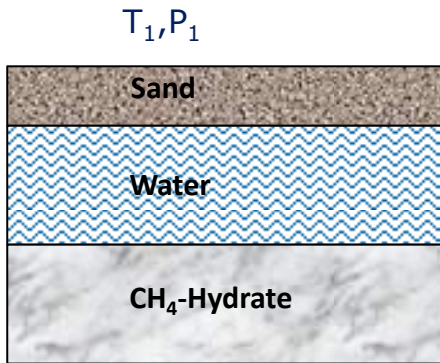
GEOMAR



# Experiment steps



GEOMAR

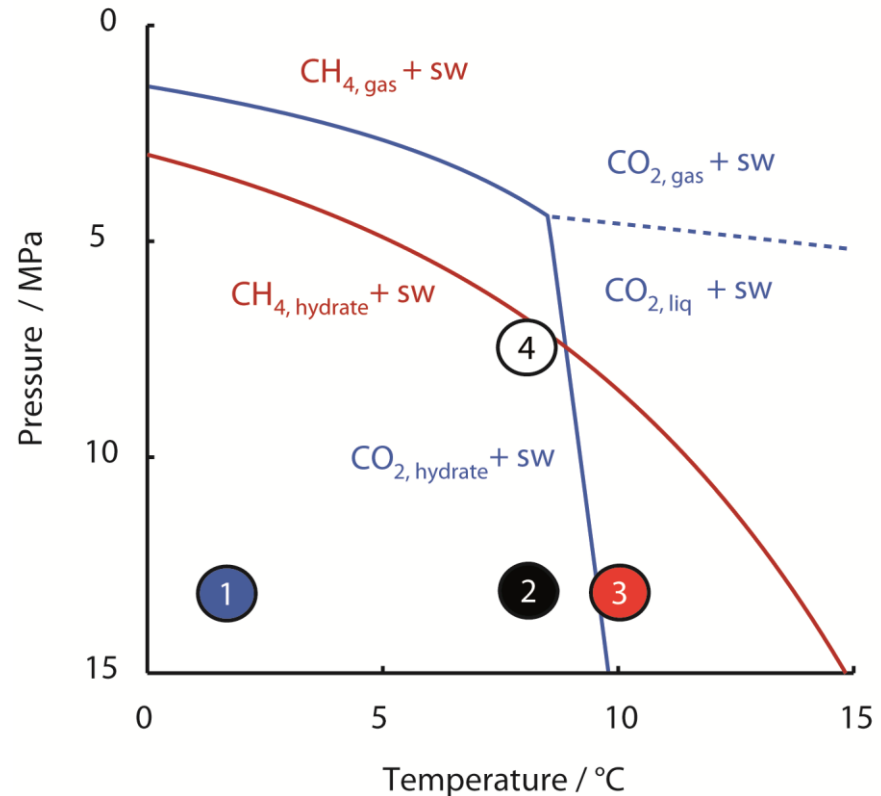


- **4 experiments at different p/T-conditions**

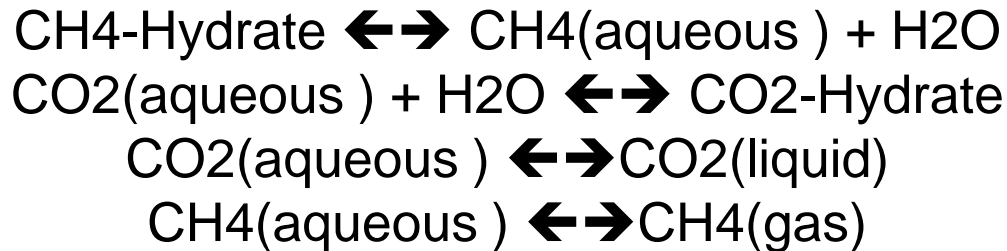
- 1) 2°C / 13 MPa
- 2) 8°C / 13 MPa
- 3) 10°C / 13 MPa
- 4) 8°C / 8 MPa

- **CO<sub>2</sub> injection**

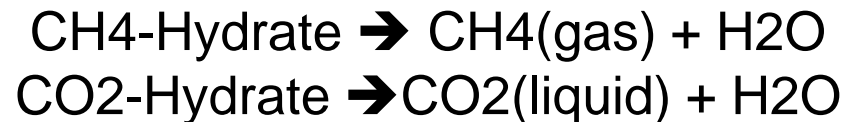
- 95°C
- 2-5 ml/min



Under stability conditions:



At dissociating conditions:

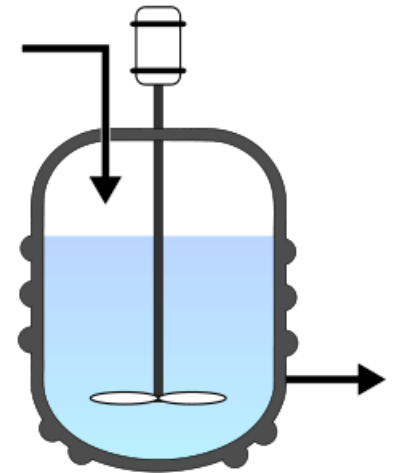


- In CSTR model, mass and energy balance are solved explicitly and coupled to the reactivity in the system.

## 1. Bulk model approach

Using CSTR (continuous stirred tank reactor) and Batch

- Assuming the reactor as a non-isothermal CSTR
- Assuming the effects caused by transport limitations are negligible or included into the estimated effective rate parameters
- All properties (T, P, concentrations) are averaged over the reactor and therefore have one value.



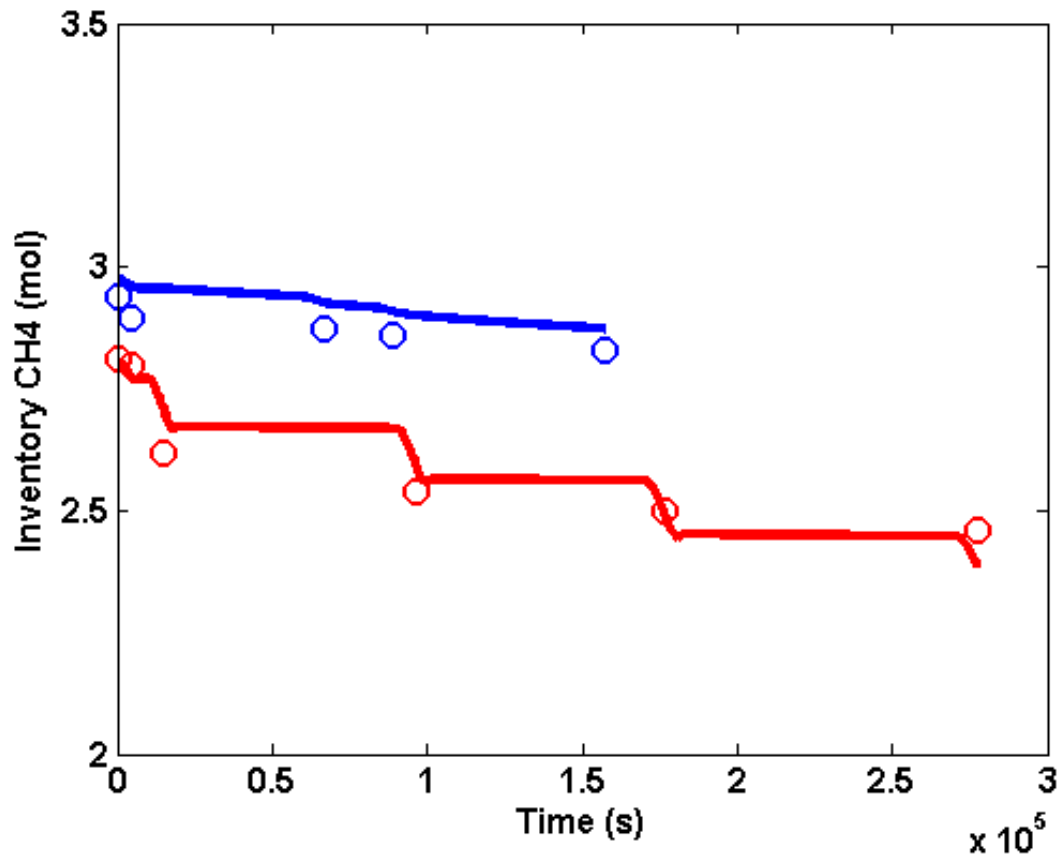
- **Pros:**

- Fast, effective and computationally cheap
- Good approximations of dynamics at small-scales
- quick and easy for sensitivity analysis
- Better numerical convergence on higher non-linearities raised by complicated definitions of reaction rates – multiple reactions

- **Cons:**

- There is one averaged value for quantities like pressure, temperature and chemical concentrations
- CSTR can not address spatial properties and thus is not precise enough for reservoir modeling
- Medium geometry, inlet and outlet positions, shape of reservoir and etc. don't influence the outcomes.
- Transport limitation effects are neglected.

# CSTR Model preliminary results



- Total CH4 in the system for **experiment 1** and **experiment 3**.

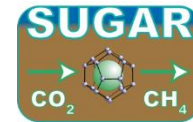
- 1) 2°C / 13 Mpa
- 3) 10°C / 13 MPa

- **CO<sub>2</sub> injection**

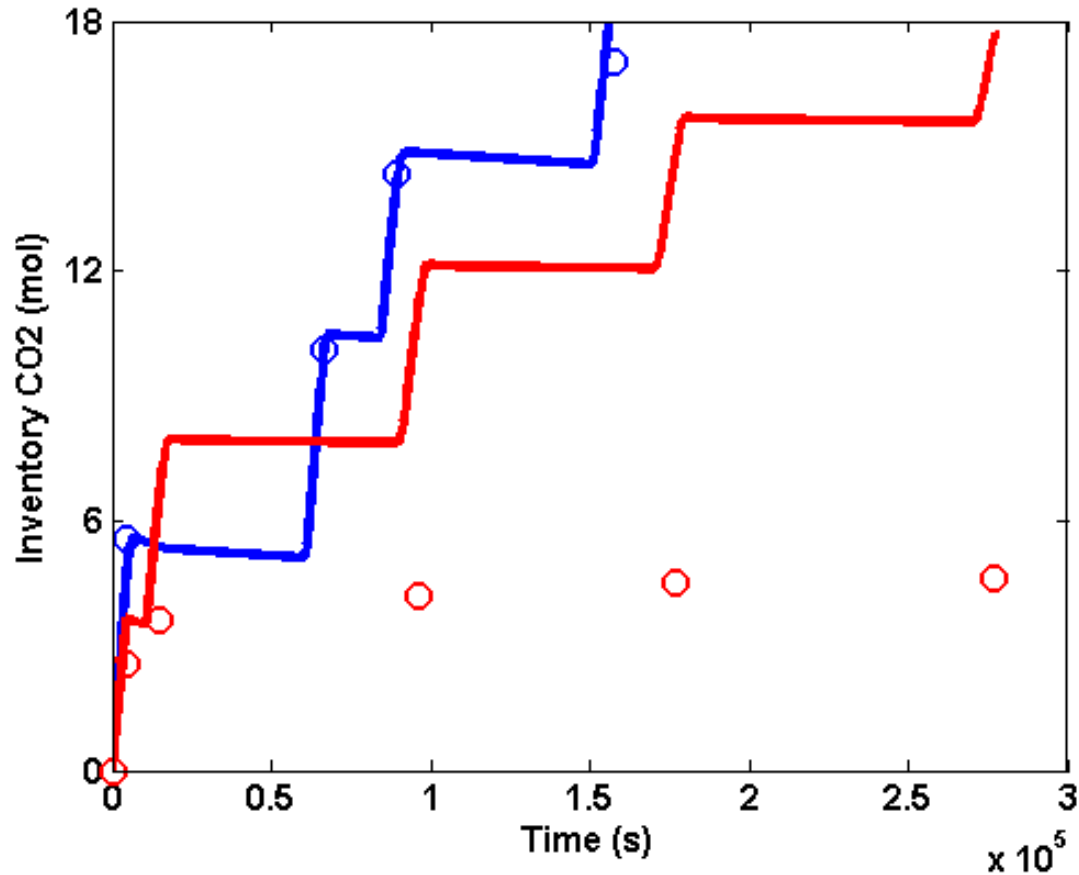
- 95°C
- 2-5 ml/min



# CSTR Model preliminary results



**GEOMAR**



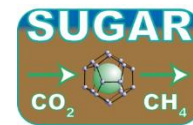
- Total CO<sub>2</sub> in the system for **experiment 1** and **experiment 3**.

- 1) 2°C / 13 Mpa
- 3) 10°C / 13 MPa

- **CO<sub>2</sub> injection**

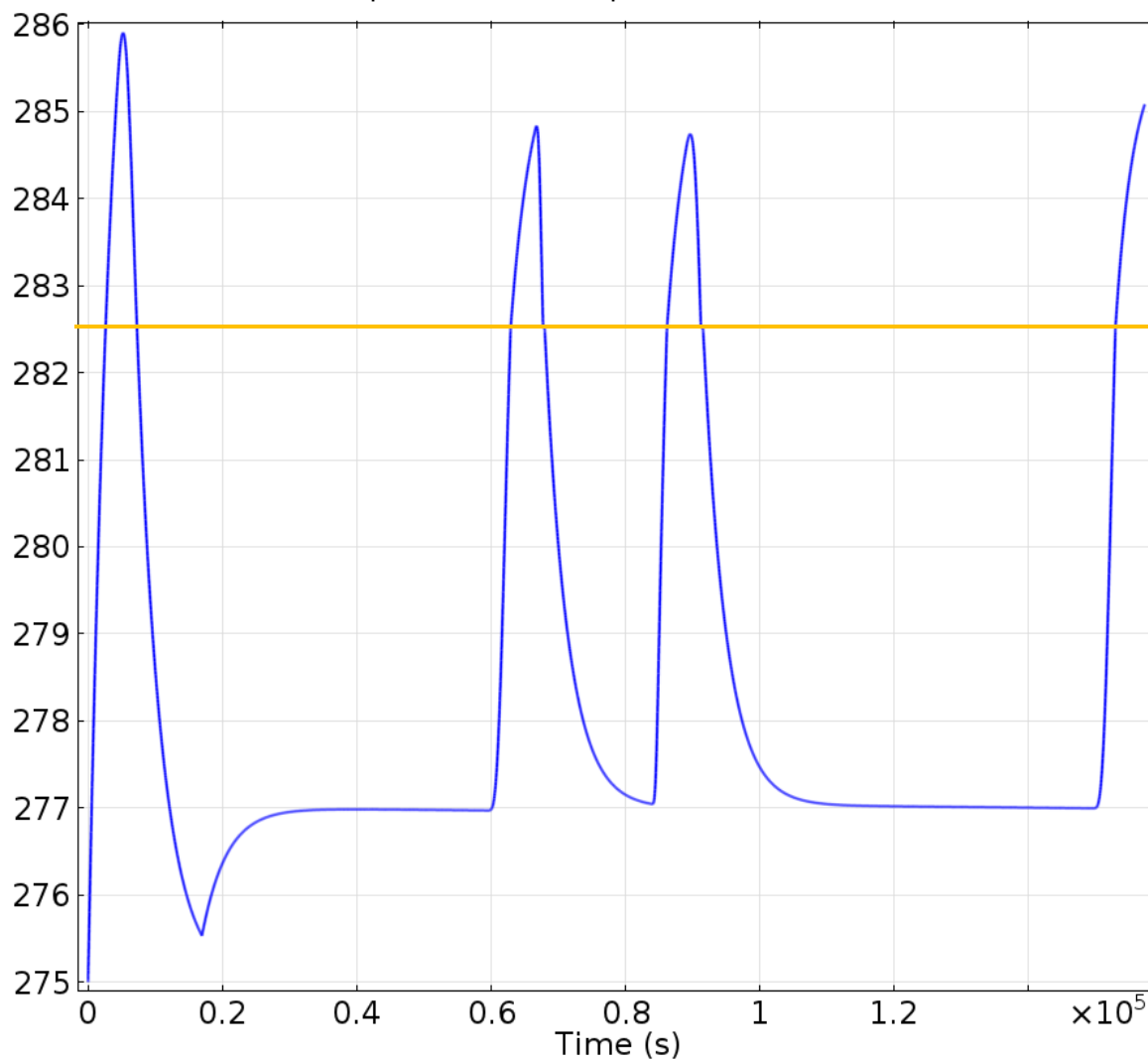
- 95°C
- 2-5 ml/min

# CSTR results for experiment 1



**GEOMAR**

Experiment 1 temperature

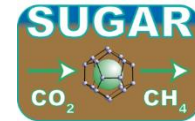


**CH<sub>4</sub> stability temperature= 287 K**

**CO<sub>2</sub> stability temperature= 282.5 K**

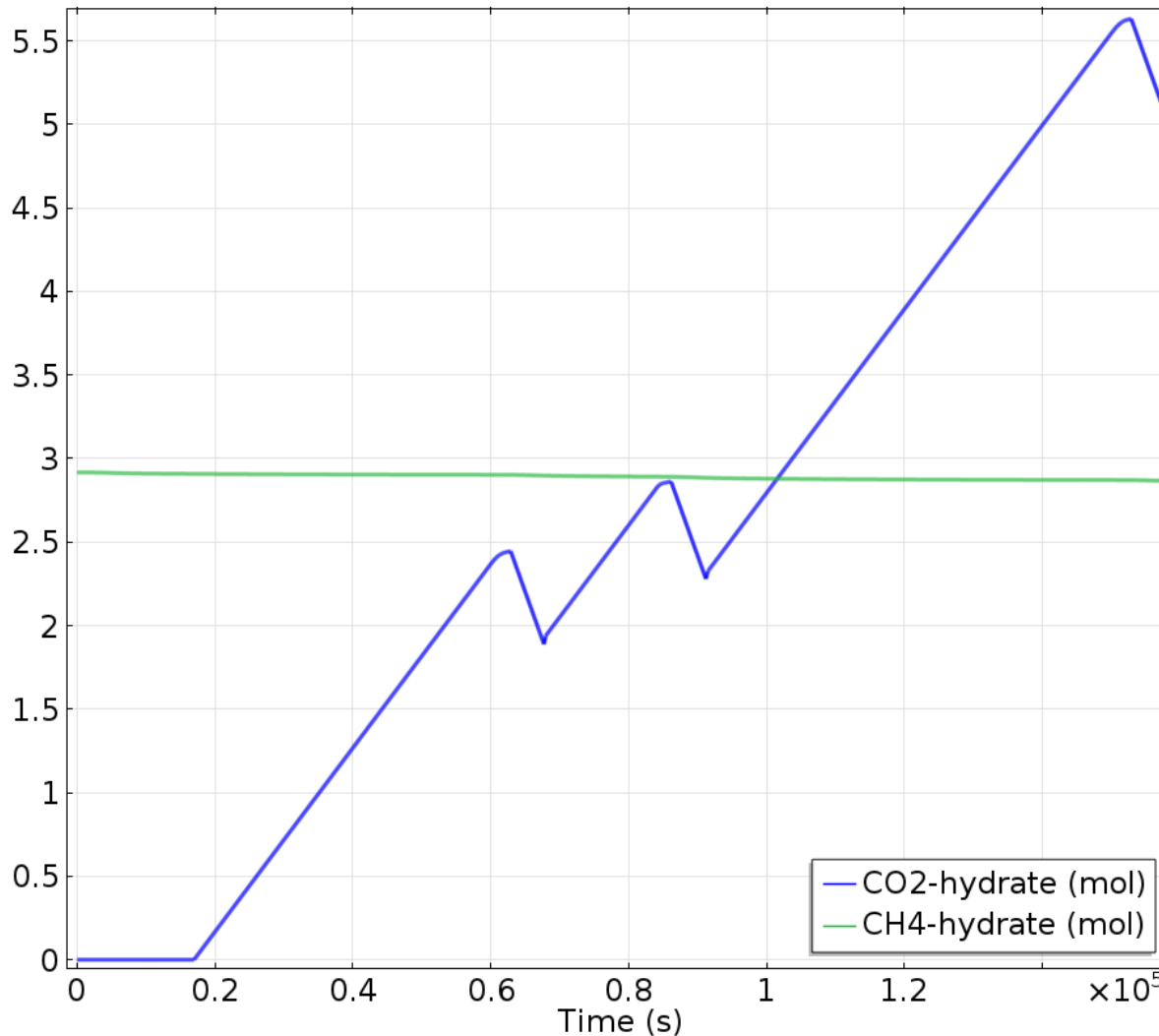
- Exp (1) 2°C / 13 Mpa
- **CO<sub>2</sub> injection**
- 95°C
- 2-5 ml/min

# CSTR results for experiment 1



**GEOMAR**

Hydrate amount in the system (Exp 1)

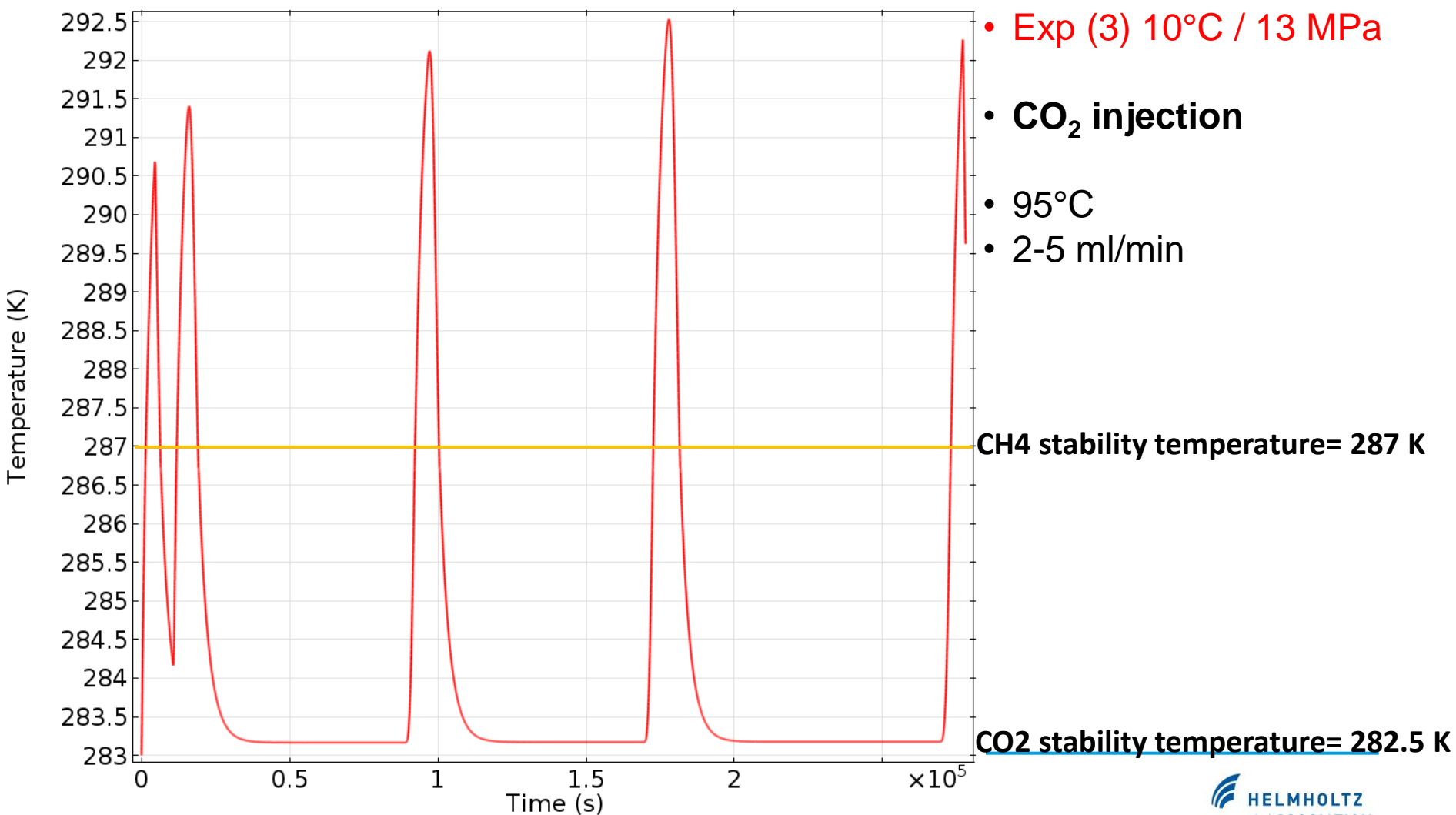


- Exp (1) 2°C / 13 Mpa
- CO<sub>2</sub> injection
- 95°C
- 2-5 ml/min

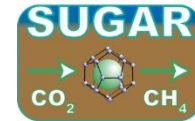
# CSTR results for experiment 3



Experiment 3 temperature

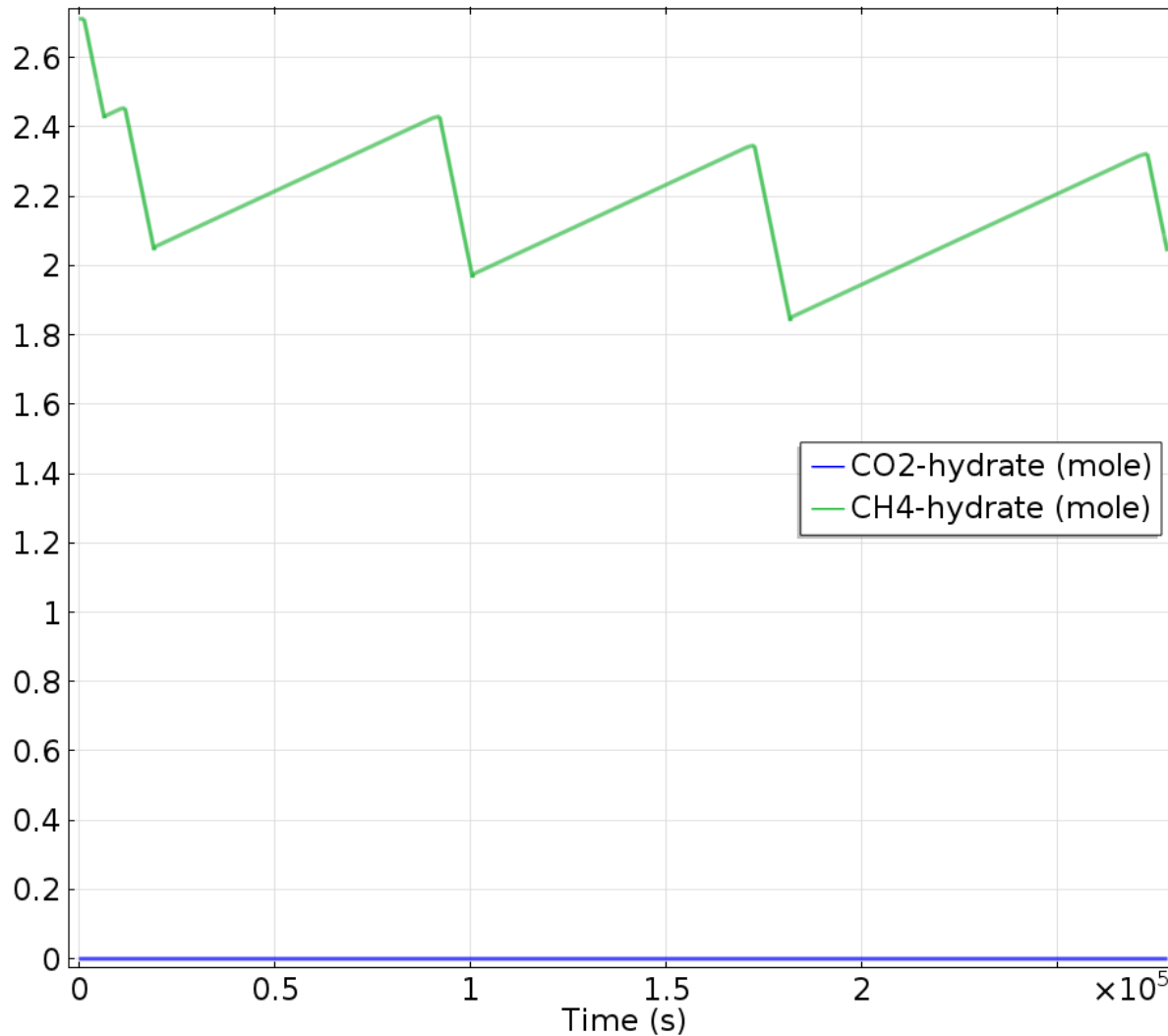


# CSTR results for experiment 3



**GEOMAR**

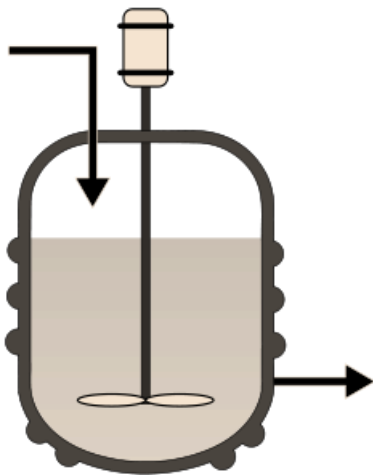
Hydrate amounts in the system (Exp 3)



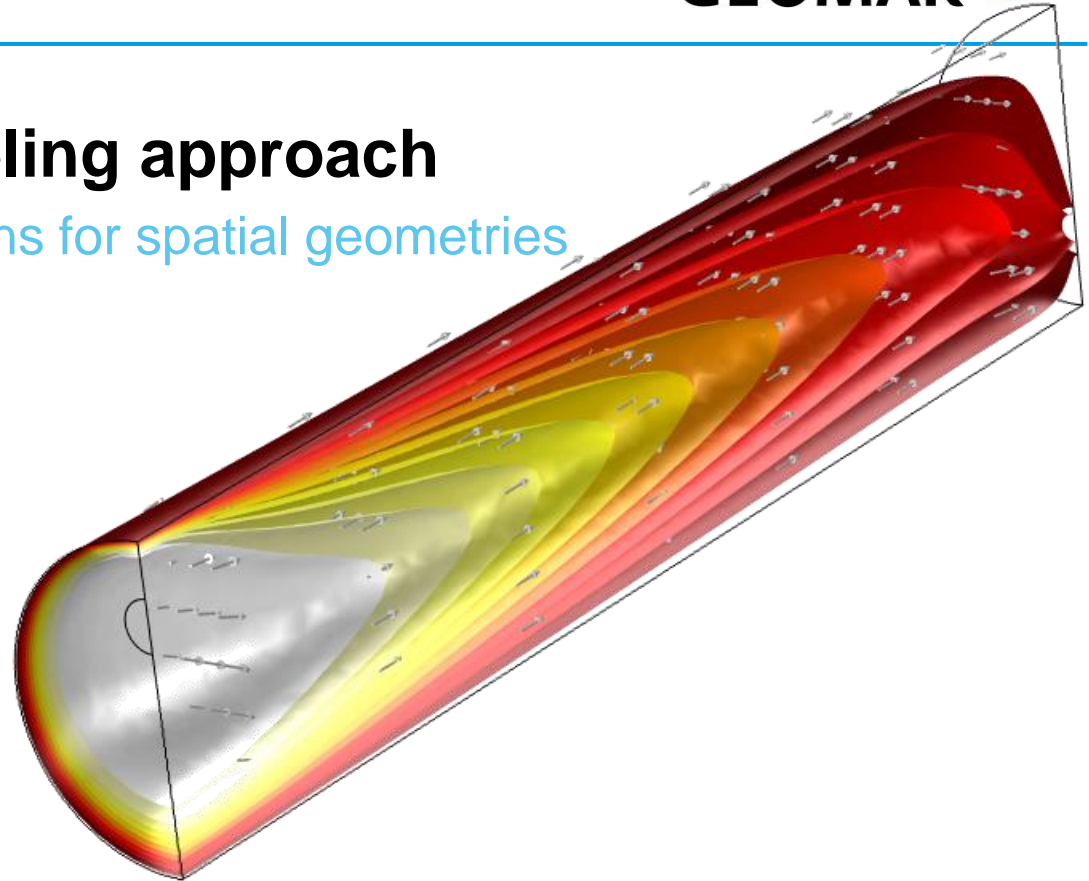
- Exp (3) 10°C / 13 MPa
- CO<sub>2</sub> injection
- 95°C
- 2-5 ml/min

## 2. Reservoir modeling approach

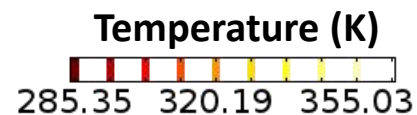
Solving the flow equations for spatial geometries



Average Temperature= 330 (K)



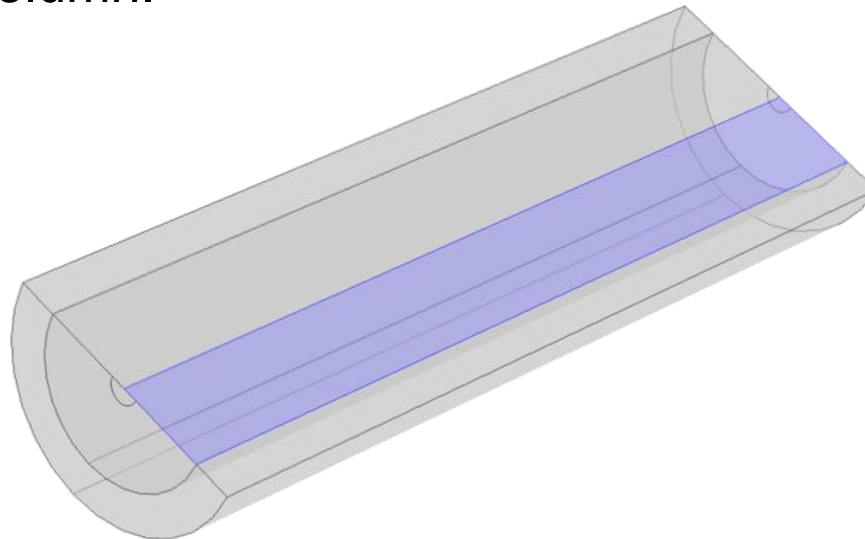
▼ 285.35



▲ 363.74

## Two-phase fluid flow transport

- In order to include the spatial movement of the components in the model, development of a two-phase platform has been started.
- In following a non-wet phase pushes the wetting phase out of an experimental column.

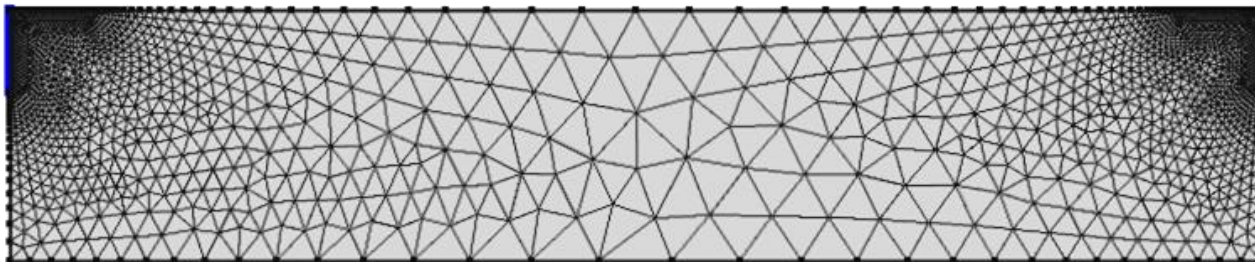


## Two-phase fluid flow

### Medium and meshing

- At inlet non-wet phase (CO<sub>2</sub>) enters the medium and wetting-phase (Water) depletes from outlet.

Hot CO<sub>2</sub> inlet (constant injection rate)



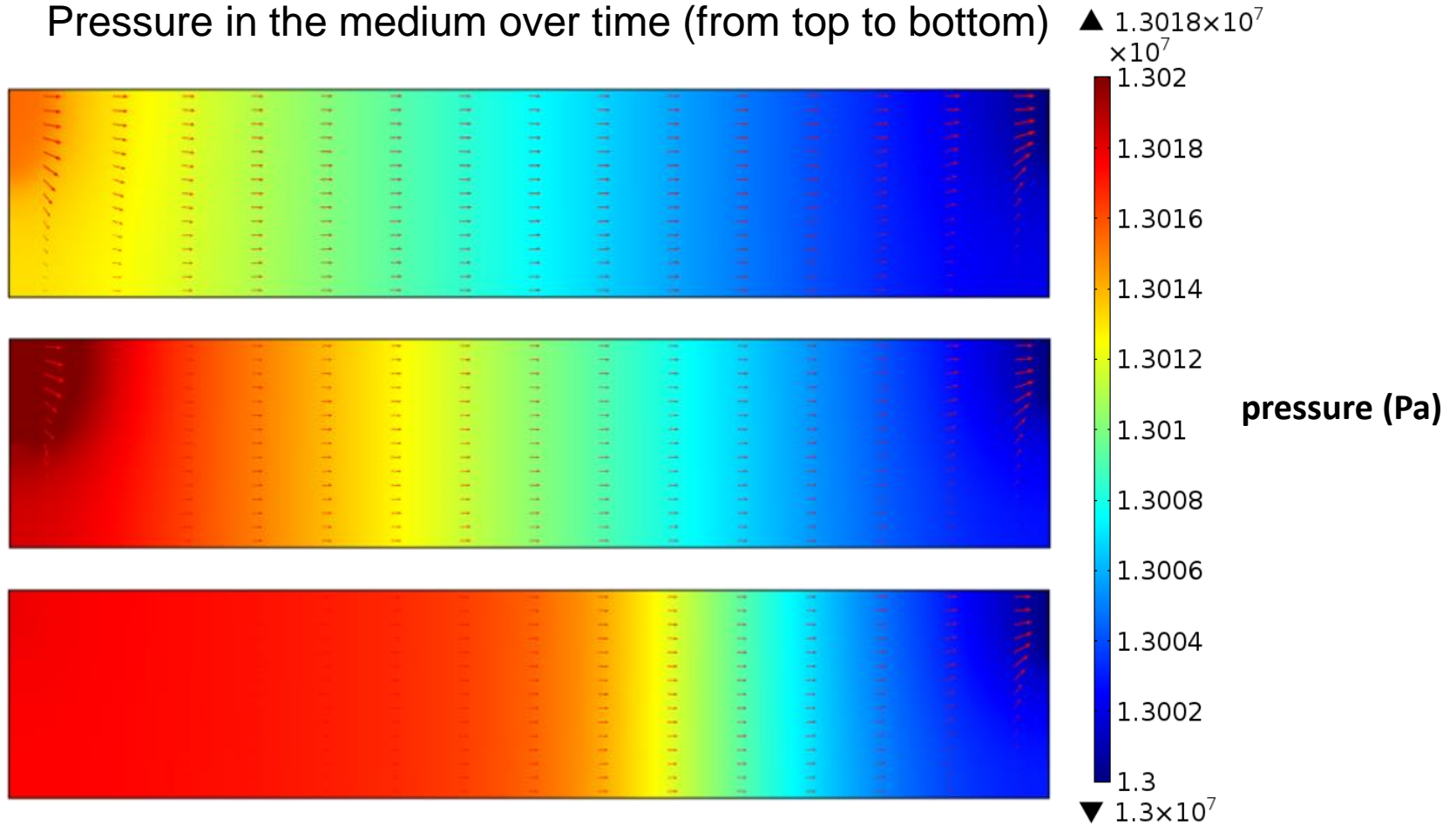
Outlet



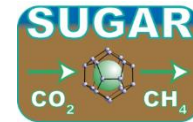


## 2-phase Model preliminary results

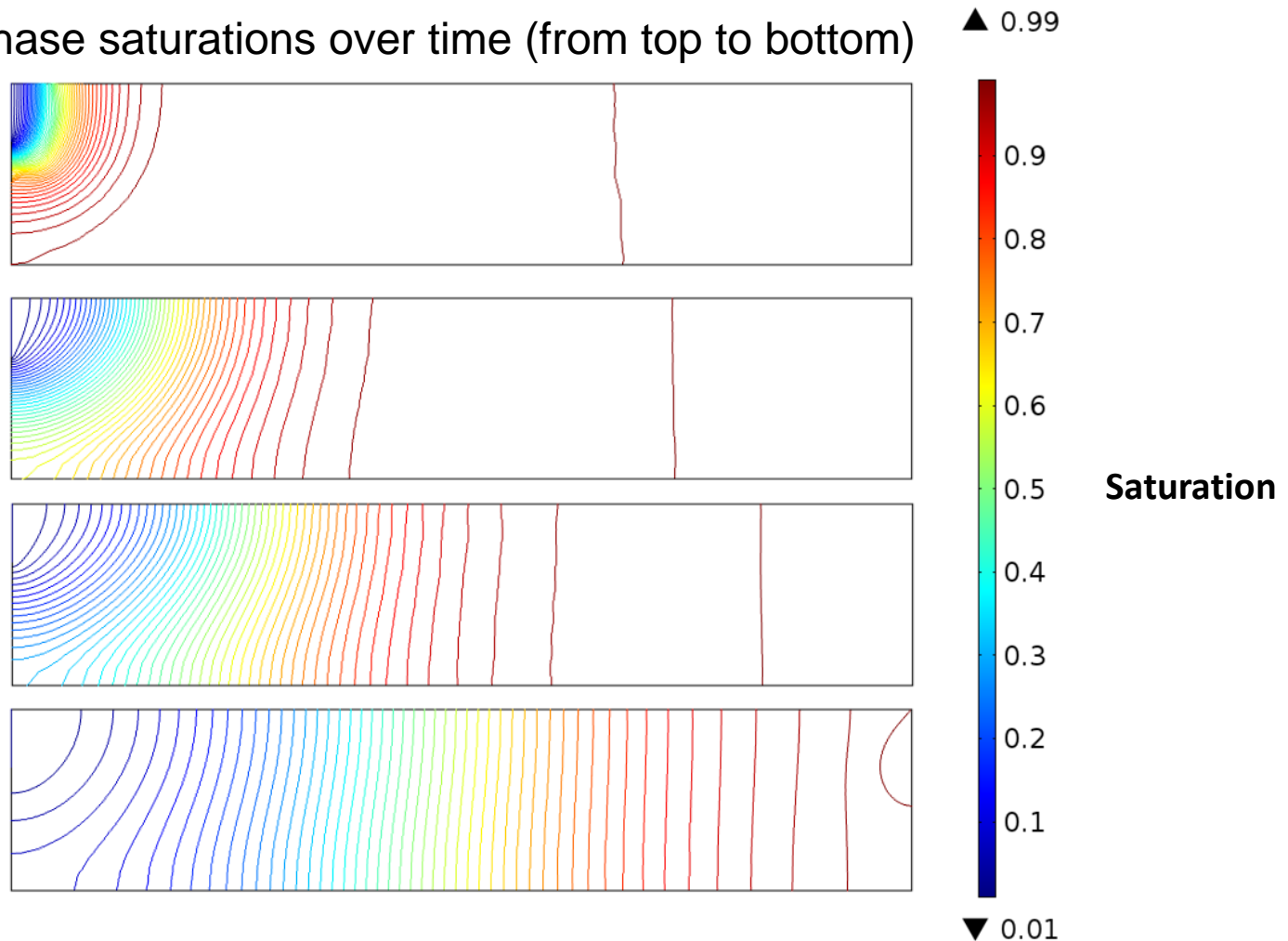
- Pressure in the medium over time (from top to bottom)



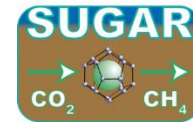
## 2-phase Model preliminary results



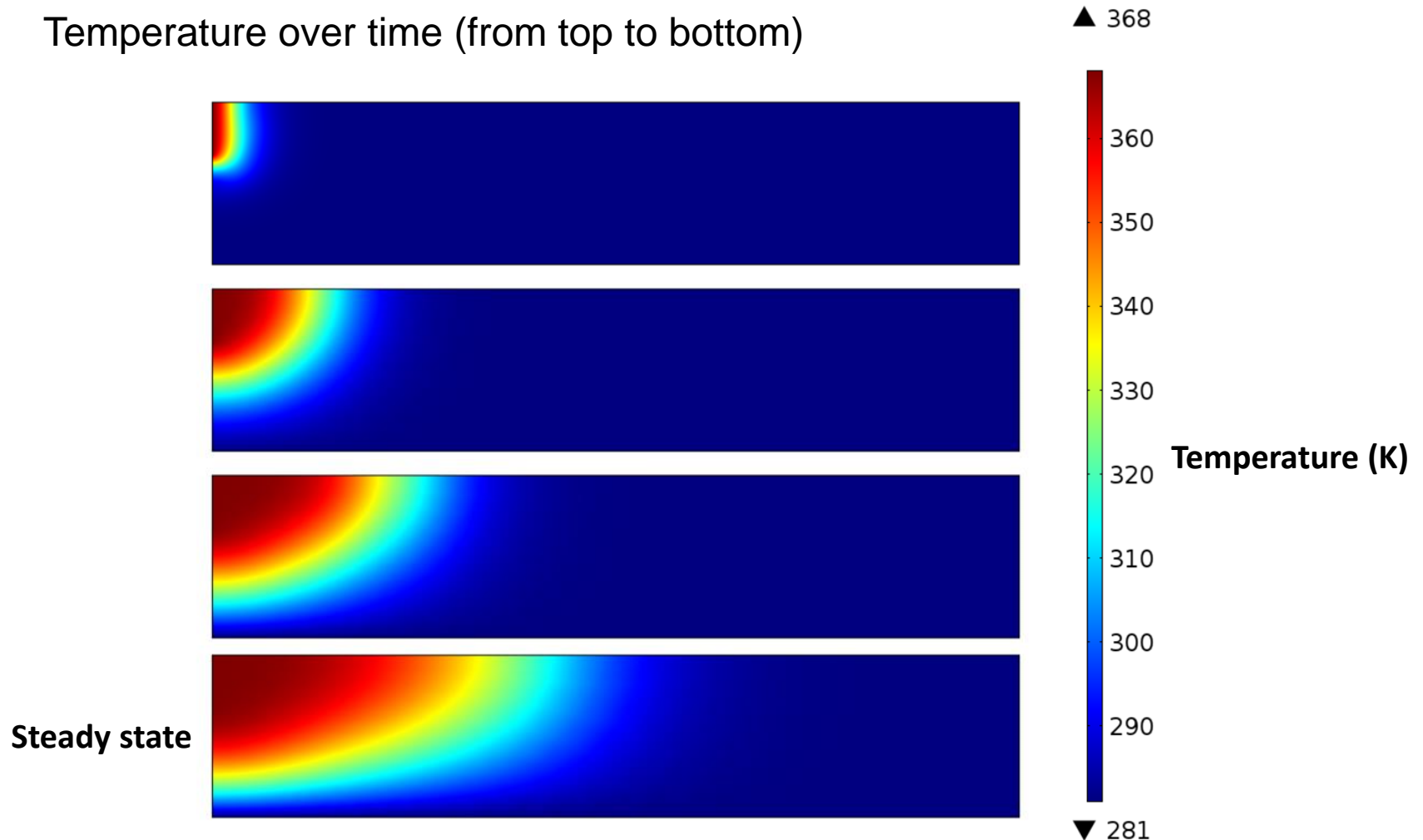
- Wetting phase saturations over time (from top to bottom)



## 2-phase Model preliminary results

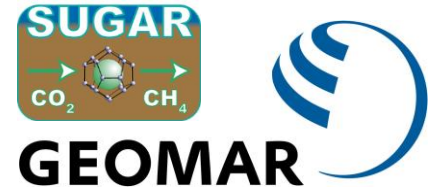


- Temperature over time (from top to bottom)



## Take-away messages

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- Two different modeling approaches for methane-hydrate dissociation were presented.
- CSTR-based model is quick and provide a platform for 3-phase solutions which are not currently feasible in reservoir models.
- Parameter study is only feasible with 2D or CSTR models since the computational time of the 3D models is very high.
- In turn, 3D models enable us to discover some details that 2D models can't show.

***Thank you for your attention and see you at Poster #8***

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