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SCIENTIFIC AND STRATEGIC ENVIRONMENTAL CONSULTING

Benchmarking tailored formulations of multiphase flow in porous media

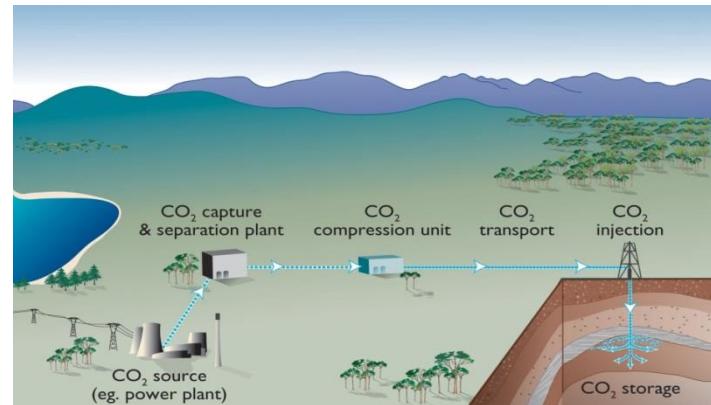
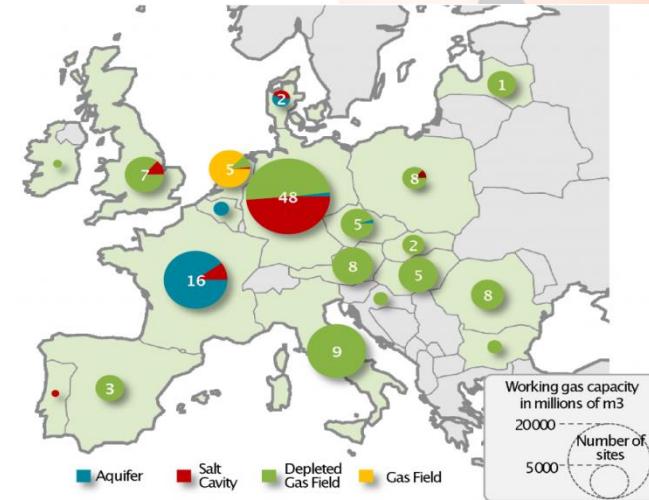
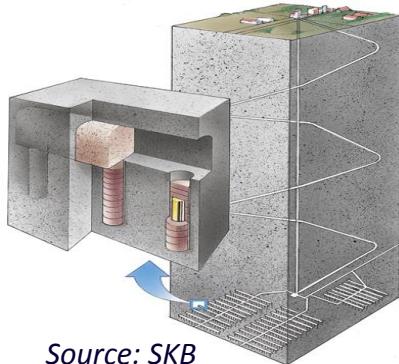
Álvaro Sáinz-García, E. Abarca, A. Nardi, F. Grandia



Multiphase flow situations

New uses of the underground

- Geological gas storage
 - Hydrogen storage
 - Carbon capture and storage
- Oil and gas industry
 - Enhance Oil Recovery
- Nuclear waste storage



ADE system

Component mass conservation

$$\partial_t(\phi S_\alpha \rho_\alpha m_\alpha^k M^\kappa) = -\nabla(\mathbf{q}_\alpha \rho_\alpha m_\alpha^k M^\kappa - \phi S_\alpha \rho_\alpha \mathbf{D}_\alpha \nabla(m_\alpha^k M^\kappa)) + Q_\alpha^\kappa + T_\alpha^\kappa$$

$$\mathbf{q}_\alpha = -\frac{k k_{r,\alpha}}{\mu_\alpha} (\nabla P_\alpha - \rho_\alpha \mathbf{g})$$

$\alpha = \text{wetting \& non-wetting phase}$

$k = \text{components}$

Typically 4 equations

Constitutive equations

Total saturation

$$S_n + S_w = 1$$

Capillarity pressure

$$\begin{cases} P_{cap} = P_n - P_w \\ P_{cap} = P_{cap}(S_w) \end{cases}$$

Relative permeability $k_l^r, k_g^r = f(S_w)$

Gas volume

$$V_g = V_g(p_g, T, m_l^{CO_2}, m_s^{NaCl})$$

Liquid density

$$\rho_b = \rho_b(p_l, T, m_l^{CO_2}, m_s^{NaCl})$$

Viscosity

$$\mu_g = \mu_g(p_g, T, m_l^{CO_2}, m_s^{NaCl})$$

...

Modeler alternatives

- How to represent the **capillary pressure**
 - Van Genuchten
 - Brooks & Corey
 - Specific interfacial area
- Which **unknowns** will be solved
 - Phase pressure & Phase saturation ($S_\alpha, P_\alpha \}$)
 - “Global” variables (total pressure or capillary pressure)
- Which **combination of governing equations** will be solved
 - Global equation, phase equation, linear combinations,...
- Which **state variables** will be used
 - Thermodynamic relations

COMSOL Implementation

Non-wetting + wetting eq.

$$0 = \nabla \left(k\lambda_n \left(\nabla P_w + \frac{dP_{cap}}{dS_n} \nabla S_n - \rho_n \mathbf{g} \nabla z \right) \right) + \nabla (k\lambda_w (\nabla P_w - \rho_n \mathbf{g} \nabla z)) + q_n + q_w$$

Non-wetting eq.

$$\phi \partial_t (S_n) = \nabla \left(k\lambda_n \left(\nabla P_w + \frac{dP_{cap}}{dS_n} \nabla S_n - \rho_n \mathbf{g} \nabla z \right) \right) + q_n$$

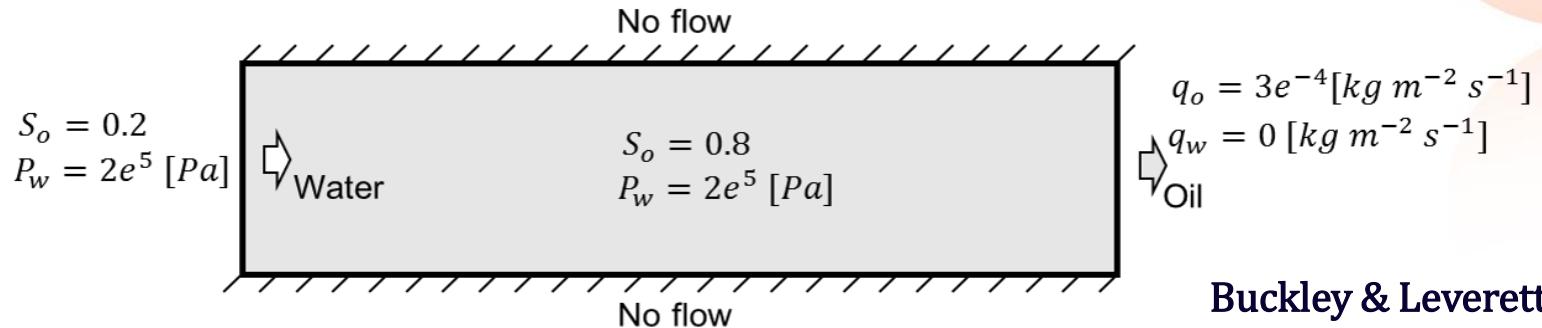
Matrix form:

$$\begin{pmatrix} 0 & 0 \\ 0 & \phi \end{pmatrix} \frac{\partial}{\partial t} \begin{pmatrix} P_w \\ S_n \end{pmatrix} + \nabla \cdot \left[-k \begin{pmatrix} \lambda & \lambda_n \frac{dP_{cap}}{dS_n} \\ \lambda_n & \lambda_n \frac{dP_{cap}}{dS_n} \end{pmatrix} \nabla \begin{pmatrix} P_w \\ S_n \end{pmatrix} - kg \begin{pmatrix} \lambda_w \rho_w + \lambda_n \rho_n \\ \lambda_n \rho_n \end{pmatrix} \right] = \begin{pmatrix} q_n + q_w \\ q_n \end{pmatrix}$$

COMSOL Coefficient Form PDE

$$e_a \frac{\partial^2 \mathbf{u}}{\partial t^2} + d_a \frac{\partial \mathbf{u}}{\partial t} + \nabla \cdot (-c \nabla \mathbf{u} - \alpha \mathbf{u} + \gamma) + \beta \cdot \nabla \mathbf{u} + a \mathbf{u} = f$$

Benchmarking – Buckley-Leverett problem



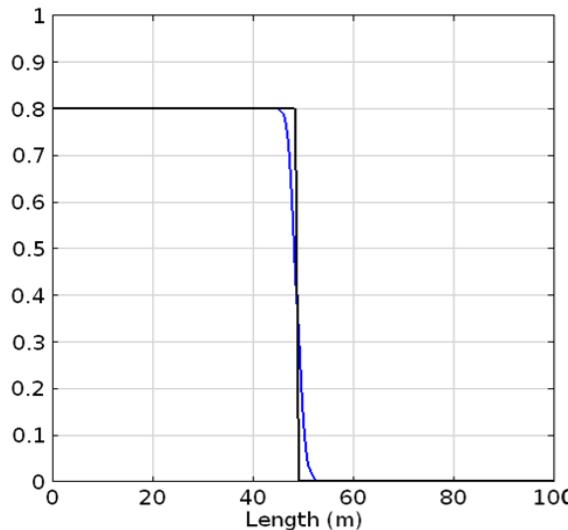
Buckley & Leverett, 1942

- 1D displacement of oil by water
- Immiscible fluids
- No capillary pressure
- Various fluid viscosities
- Gravity effects neglected
- Homogeneous porous media

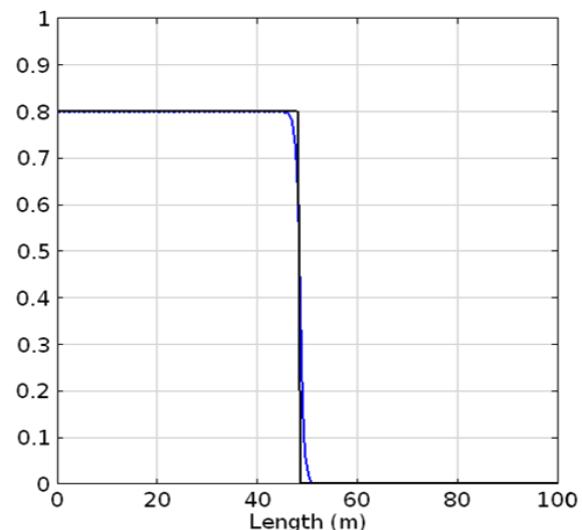
Benchmarking – Buckley-Leverett problem

Water Saturation after 300 days

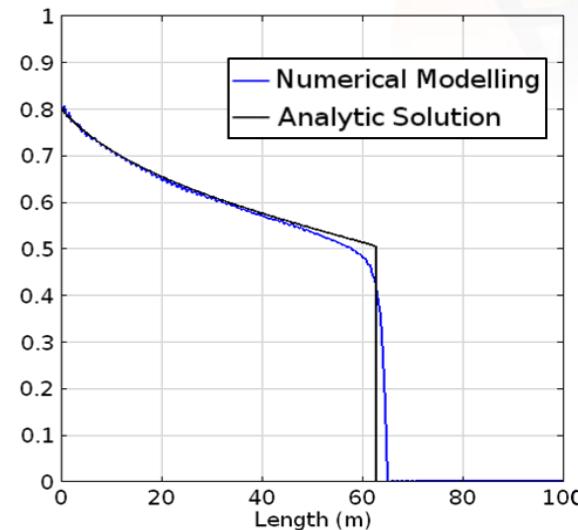
$$\mu_w/\mu_o = 1$$



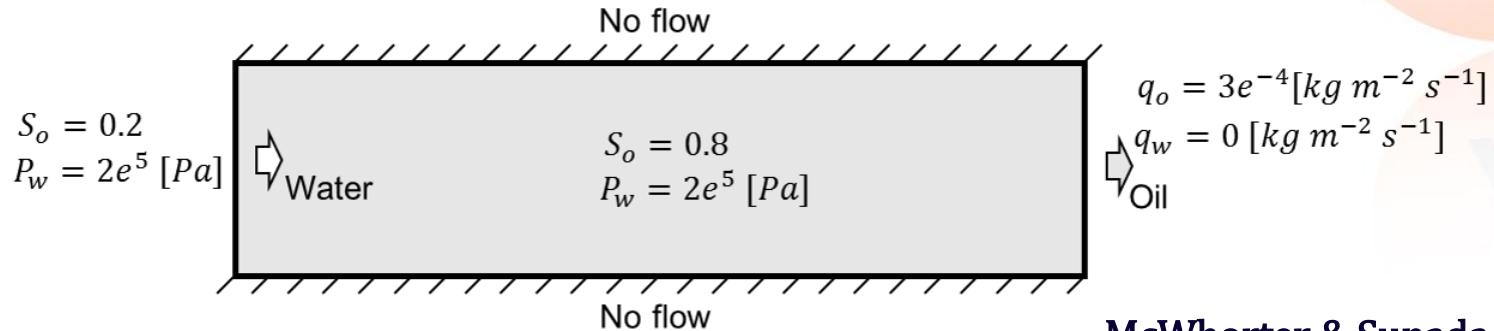
$$\mu_w/\mu_o = 2$$



$$\mu_w/\mu_o = 2/3$$



Benchmarking – McWorther problem

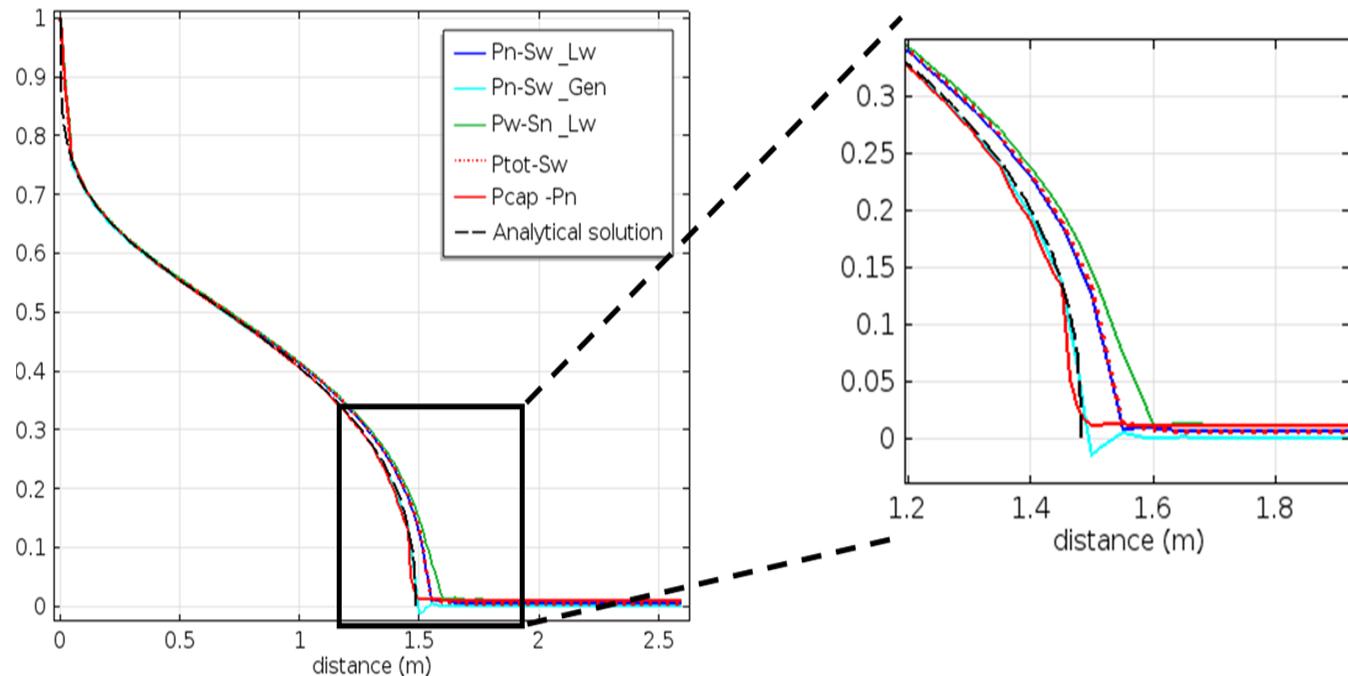


McWhorter & Sunada, 1990

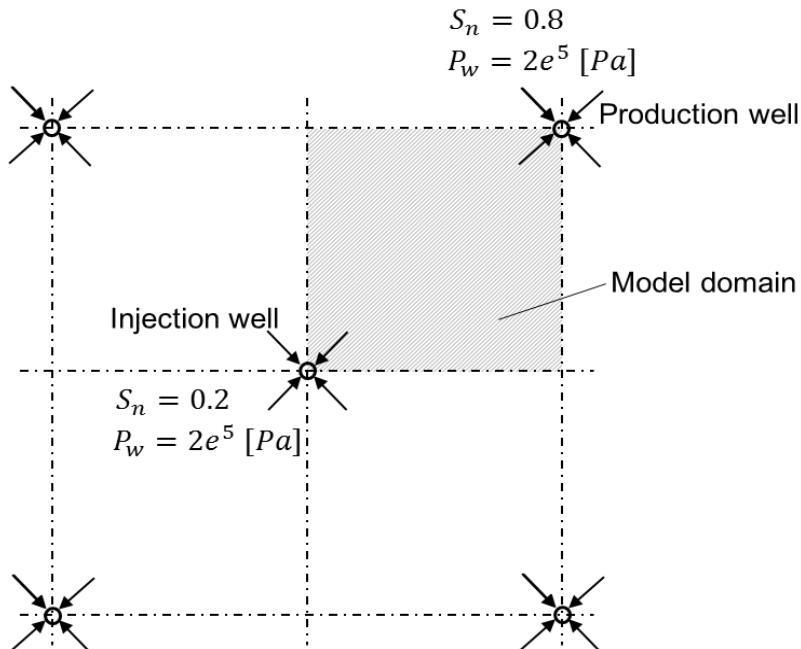
- 1D displacement of oil by water
- Immiscible fluids
- Capillary pressure
- Equal fluid viscosities
- Gravity effects neglected
- Homogeneous porous media

Benchmarking – McWorther problem

Water Saturation after 2.78 hours



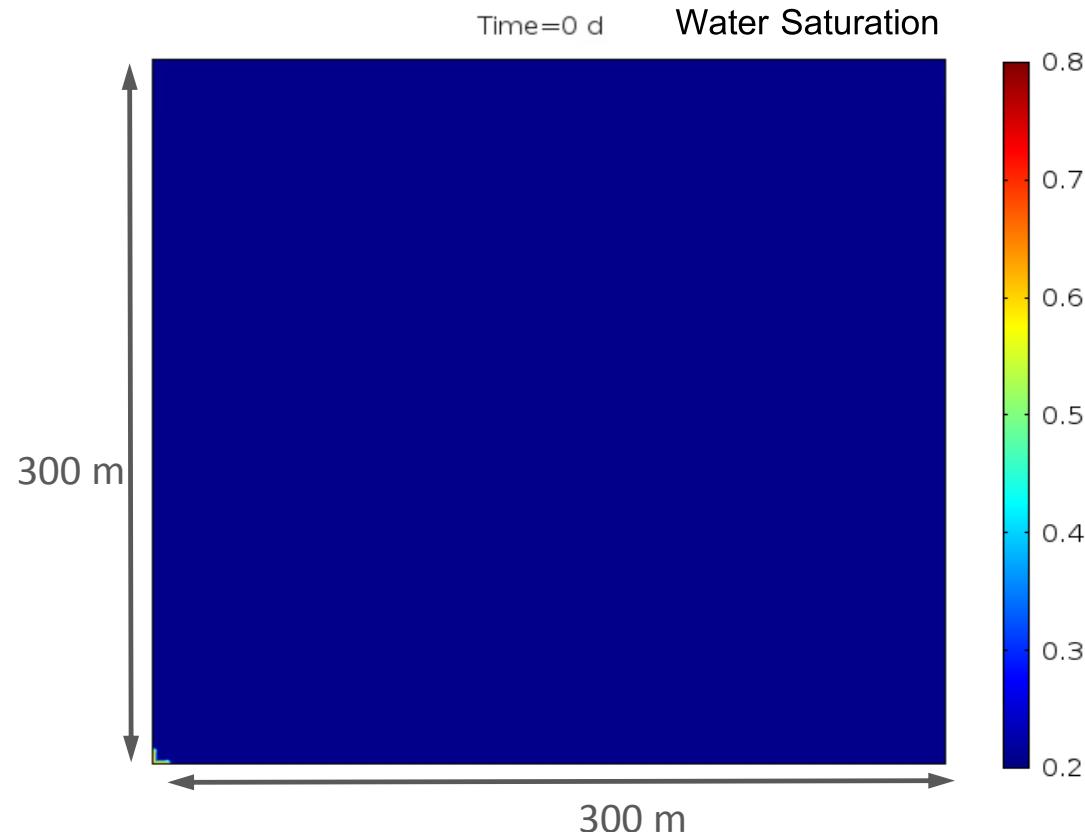
Benchmarking – Five spot problem



Chen, et al., 2006

- 2D displacement of oil by water
- Immiscible fluids
- No capillary pressure
- Equal fluid viscosities
- Gravity effects neglected
- Homogeneous porous media

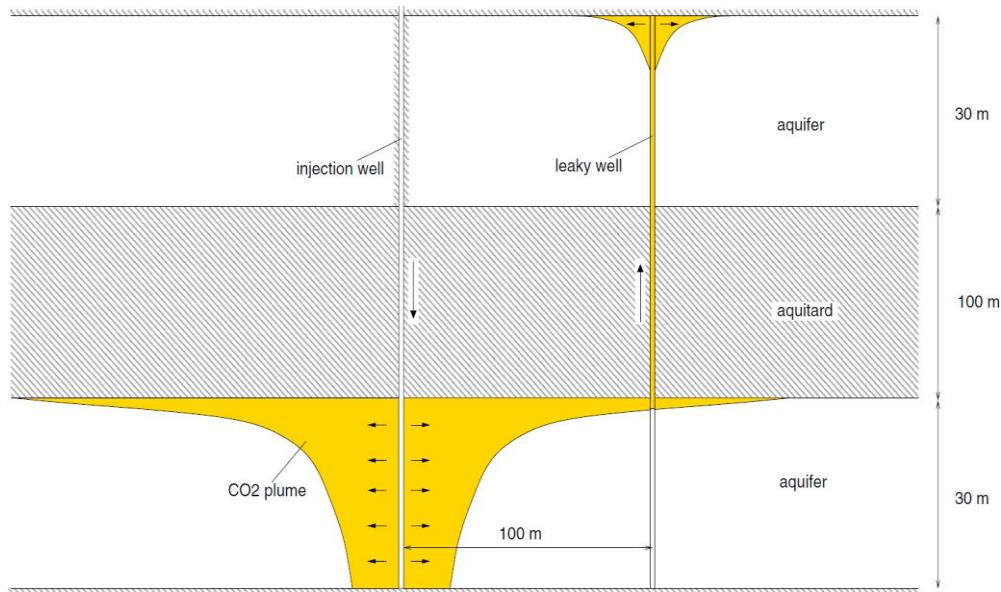
Benchmarking – Five spot problem



Multiphase flow

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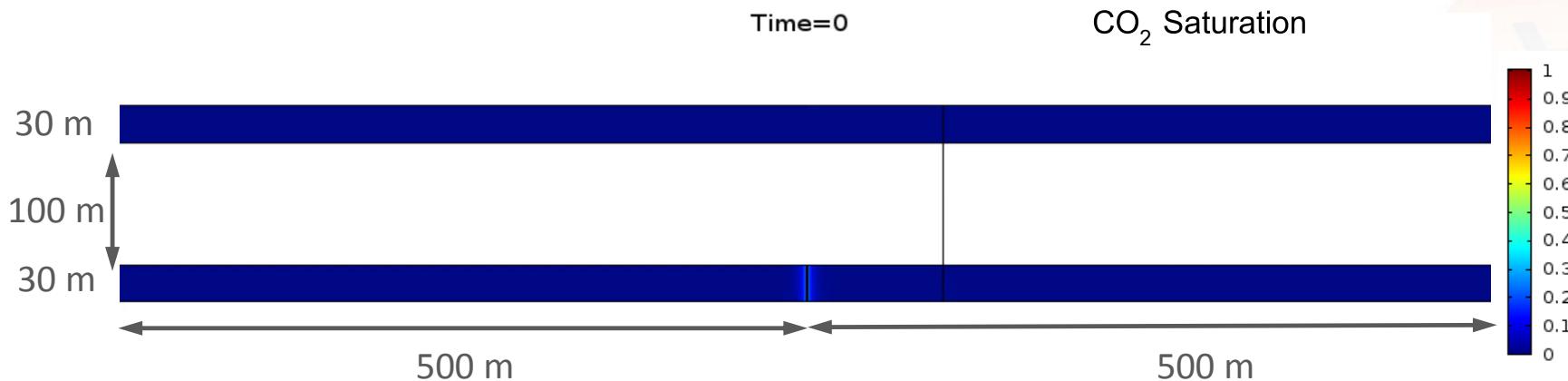
Benchmarking – CCS well leakage



Ebigbo et al., 2007

- 2D model simplification of the 3D problem
- Immiscible fluids
- No capillary pressure
- ρ, μ are constant
- isothermal

Benchmarking – CCS well leakage



Summary

- Formulations reproduced multiphase physical processes
- equations of state of oil, water, brine and CO₂^{sup}
 - easily extended to any other fluid
- The manner the equations are combined matters
- **Each formulation has its own benefits and drawbacks**
- The preferred may vary depending on the physics and numerical methods

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